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INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

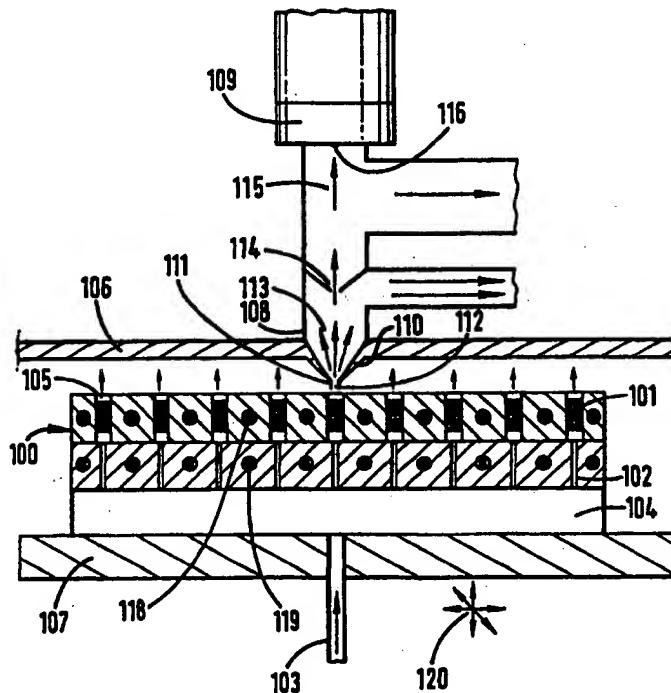
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(71) Applicants (for all designated States except US): BP CHEMICALS LIMITED [GB/GB]; Britannic House, 1 Finsbury Circus, London EC2M 7BA (GB). LASER CATALYST SYSTEM INC. [US/US]; 11000 Wilshire Boulevard, Box 24314, Los Angeles, CA 90024 (US).	
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(73) Inventor/Applicant (for US only): SENKAN, Selim, Mehmet [US/US]; 1269 Warner Avenue, Los Angeles, CA 90024 (US).	
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(54) Title: METHOD AND APPARATUS FOR SCREENING CATALYST LIBRARIES

(57) Abstract

Rapid screening for activities and selectivities of catalyst libraries having addressable test sites is achieved by contacting potential catalysts at the test sites with reactant streams forming product plumes at the addressable test sites. The product plumes are screened by translating a sample probe and/or the library to a position that one addressable site is in proximity to the sampling probe sample orifice and passing a portion of the reaction products through the sampling orifice forming a free jet expanded volume in at least one vacuum stage and passing a portion of the cooled and reduced pressure jet stream through an inlet orifice of a mass spectrometer for analysis. The mass spectrometric analysis may be combined with resonance enhanced multiphoton ionization methods of detection for very rapid library evaluation. Suitable reactors, microreactors, and product transfer sample micropipes for product transfer to a mass spectrometer are disclosed.





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(60) Parent Application or Grant BP CHEMICALS LIMITED [/]; (O) LASER CATALYST SYSTEM INC. [/]; (O) SENKAN, Selim, Mehmet [/]; (O) SENKAN, Selim, Mehmet [/]; (O) COLLINS, Frances, Mary; (O)			

(54) Title: METHOD AND APPARATUS FOR SCREENING CATALYST LIBRARIES

(54) Titre: PROCEDE ET DISPOSITIF PERMETTANT D'EXPLORER DES BIBLIOTHEQUES DE CATALYSEURS

(57) Abstract

Rapid screening for activities and selectivities of catalyst libraries having addressable test sites is achieved by contacting potential catalysts at the test sites with reactant streams forming product plumes at the addressable test sites. The product plumes are screened by translating a sample probe and/or the library to a position that one addressable site is in proximity to the sampling probe sample orifice and passing a portion of the reaction products through the sampling orifice forming a free jet expanded volume in at least one vacuum stage and passing a portion of the cooled and reduced pressure jet stream through an inlet orifice of a mass spectrometer for analysis. The mass spectrometric analysis may be combined with resonance enhanced multiphoton ionization methods of detection for very rapid library evaluation. Suitable reactors, microreactors, and product transfer sample micropipettes for product transfer to a mass spectrometer are disclosed.

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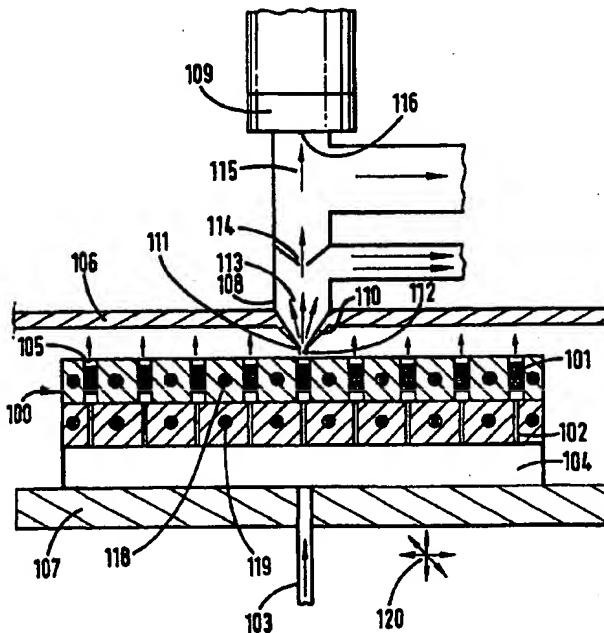
L'invention concerne un procédé permettant d'explorer rapidement les activités et les sélectivités de bibliothèques de catalyseurs ayant des sites adressables par mise en contact de catalyseurs potentiels, aux sites d'essai, avec des flux réactifs formant des plumes de produits au niveau de ces sites. On analyse les plumes de produits en transférant une sonde échantillon et/ou la bibliothèque à une position telle qu'un site adressable soit proche de l'orifice d'échantillonage de la sonde échantillon, puis en faisant passer une partie des produits de réaction par cet orifice, de manière à former un volume étendu de jet libre dans au moins une zone de vide et à faire passer ensuite une partie du jet sous pression refroidi et réduit par l'orifice d'admission d'un spectromètre de masse aux fins d'analyse. Il est possible de combiner cette analyse avec tel ou tel procédé de détection en ionisation multiphotonique améliorée par résonance pour assurer une évaluation très rapide des bibliothèques. L'invention concerne également des réacteurs, des microréacteurs et des microsondes échantillons de transfert de produit que l'on peut utiliser de manière appropriée pour le transfert de produits vers un spectromètre de masse.

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Rapid screening for activities and selectivities of catalyst libraries having addressable test sites is achieved by contacting potential catalysts at the test sites with reactant streams forming product plumes at the addressable test sites. The product plumes are screened by translating a sample probe and/or the library to a position that one addressable site is in proximity to the sampling probe sample orifice and passing a portion of the reaction products through the sampling orifice forming a free jet expanded volume in at least one vacuum stage and passing a portion of the cooled and reduced pressure jet stream through an inlet orifice of a mass spectrometer for analysis. The mass spectrometric analysis may be combined with resonance enhanced multiphoton ionization methods of detection for very rapid library evaluation. Suitable reactors, microreactors, and product transfer sample micropipes for product transfer to a mass spectrometer are disclosed.		

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Description

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METHOD AND APPARATUS FOR SCREENING CATALYST LIBRARIES

20 This invention relates to rapid screening for activities and selectivities of heterogeneous and homogeneous catalyst libraries by mass spectrometry. This invention provides very rapid screening of gaseous, liquid or solid products from all catalyst sites in a catalyst library by mass spectrometry and its combination with selective resonance 25 enhanced multiphoton ionization (REMPI).

30 Solid and liquid catalysts are used in the manufacture of a vast array of chemicals and fuels, and in this manner significantly contribute to the economy and high living standards. National Research Council, "Catalysis Looks to the Future", National Academy Press, Washington, D.C., 1992. Catalysts also provide important 10 environmental benefits, such as in catalytic converters for internal combustion engines. However, in spite of their significance and broad utility, the development of new and improved catalysts continues to be an arduous and rather unpredictable trial and error 35 process. Conventionally, an individual catalyst is prepared using a large variety of tedious and time consuming methods, characterized and tested for catalytic activity, 40 modified, again characterized and tested again, until no further improvements are justified. This approach, although time consuming, has been successful for the discovery of a significant number of solid state catalysts, Heinemann, H., "A Brief History of 45 Industrial Catalysts", Catalysis: Science and Technology, Anderson, J.R. and Boudart, M. Eds., Chapter 1, Springer-Verlag, Berlin, 1981, and homogeneous, liquid-state 20 catalysts, Montreus, A. and Petit, F., "Industrial Applications of Industrial Catalysts" 50 Kluwer Publishing, New York, 1988.

55 Combinatorial chemistry, in which a large number of chemical variants are

5 produced rapidly and a chemical library generated which is then screened for desirable properties using a suitable technique, is a particularly attractive approach for the discovery of new catalysts. Chem. Eng. News, 12 Feb. 1996. Combinatorial synthesis was initially used to synthesize large libraries of biological oligomers, such as peptides

10 5 and nucleotides, however, the creation of small molecule libraries which can be used for drug testing is growing. Nielsen, J., Chem. & Indus., 902, 21 Nov. 1994. Recently, combinatorial diversity synthesis has been extended to solid-state compounds used in

15 superconducting, Xiang, X-D., Sun, X., Briceno, G., Lou, Y., Wang, K-A., Chang, H., Wallace-Freedman, W.G., Chen, S-W. and Schultz, P.G., "A Combinatorial Approach to

20 10 Materials Discovery", Science, 268, 1738, 1995, magnetoresistivity, Briceno, G., Chang, H., Sun, X., Schultz, P.G. and Xiang, X-D., "A Class of Cobalt Oxide Magnetoresistance Materials Discovered With Combinatorial Synthesis" Science, 270, 273, 1995 and luminescence, Wang, J., Yoo, Y., Takeuchi, I., Sun X-D., Chang, H., Xiang, X-D. and Schultz, P.G., "Identification of Blue Photoluminescent Composite

25 15 Material from a Combinatorial Library", Science 279, 1712, 1998, Danielson, E., Golden, J.H., McFarland, E.W., Reaves, C.M., Weinberg, W.H., and Wu, X-D., "A Combinatorial Approach to the Discovery and Optimization of Luminescent Materials",

30 Nature, 398, 944, 1997, Sun, X-D, Gao, C., Wang, J. and Xiang, X-D., "Identification and Optimization of Advanced Phosphors using Combinatorial Libraries", App.Phys.Lett., 70, 3353, 1997 and Sun, X-D., Wang, K.A., Yoo, Y., Wallace-Freedman, W.G., Gao, C., Xiang, X-D. and Schultz, P.G., "Solution-Phase Synthesis of Luminescent Materials

35 20 Libraries", Adv.Mater, 9, 1046, 1997. In these cases physically masked individual specimens were each measured using contact probes with a computer-controlled multichannel switching system. Microprobe sampling coupled to mass spectrometry,

40 25 Kassem, M., Qum, M. and Senkan, S.M., "Chemical Structure of Fuel-Rich 1,2-C₂H₄Cl₂/CH₄/O₂/Ar Flames: Effects of Microprobe Cooling on Sampling of Flames of Chlorinated Hydrocarbons", Combust. Sci. Tech., 67, 147, 1989, and in situ IR, Moates, F.C., Somani, M., Annamalai, J., Richardson, J.T., Luss, D. and Wilson, R.C., "Infrared

45 30 Thermographic Screening of Combinatorial Libraries of Heterogeneous Catalysts", Ind. Eng. Chem. Res., 35, 4801, 1996, have been proposed for catalyst screening, but suffer serious deficiencies in not having sufficient sensitivity, selectivity, spatial resolution or high throughput capacity to screen large catalyst libraries, as well as the lack of ability to

5 test the activity of hundreds or thousands of compounds simultaneously. Service, R.F.,
"High Speed Materials Design", Science, 277, 474, 1997. Microprobe mass
10 spectrometry requires sampling and transfer of very small quantities of gases containing
low concentrations of product species from each site rendering the process impractical
15 5 for rapid screening. In situ infrared techniques cannot provide information on product
selectivity which is crucial for catalyst identification.

15 Mass spectrometry is a well established and broadly applicable method for
determining mass of gaseous species. The technique involves the ionization of gaseous
molecules by a number of methods, such as, for example, by electron impact or light
20 10 photoionization followed by separation of ions using techniques, such as, for example,
quadrupole mass spectrometry or time of flight mass spectrometry and detection of
selected ions by a suitable detector. Capillary probe sampling mass spectrometry has
recently been reported for screening of catalyst libraries by Cong, P.; Giaquinta, D.;
25 Guan, S.; McFarland, E.; Self, K.; Turner, H.; and Weinberg, W. H., "A combinatorial
15 Chemistry Approach to Oxidation Catalyst Discovery and Optimization", Process
Miniaturization Section, 2nd Intl. Conf. Micro Technol., March 9-12, 1998, New
Orleans, La., pg. 118. Cong, et al teach introduction of reactant gas to an individual
30 library site through an annular space surrounding a capillary tube through which product
gas flows from that library site to the ionization zone of a mass spectrometer. Cong, et al
20 report measurement of 144 library sites in about 2 hours. Sample transfer rates by
capillary in the Cong, et al method are limited by the pumping speed tolerated by the
35 mass spectrometer chamber. Another disadvantage of capillary probe sampling is the
potential of adsorption and catalysis induced by relatively long transfer line surfaces.
There remains a large unexplored universe of binary, ternary, quaternary and higher-
40 25 order solid state materials, organometallic species and other complex metal compounds
that could have superior catalytic properties. Prior conventional approaches have been
inadequate to rapidly synthesize and screen this vast universe of catalytic compounds.
There is clearly a need for development or more efficient and systematic methods to
45 30 produce heterogeneous and homogeneous state libraries and to screen them for desired
catalytic properties. Combinatorial solid state synthesis techniques have not been applied
to the discovery of new and/or improved catalysts. A significant impediment for this has
been the lack of a broadly applicable, sensitive, selective and high throughput

5 measurement technique which could be used to rapidly screen large catalysts libraries.
Catalyst screening requires the unambiguous detection of the presence of a specific
10 product molecule in the vicinity of a small catalyst site on a large library, unlike
superconductivity or magnetoresisitivity which can both be easily tested by conventional
15 contact probes, or luminescence that can be tested by light emission.

10 This invention provides a high-throughput method to rapidly screen the activities
and selectivities of homogeneous and heterogeneous catalyst libraries generated by
15 combinatorial synthesis. Solid and liquid state catalyst libraries can be generated using a
variety of techniques and can involve the combination of a large number of chemical
20 elements and compounds.

20 In one embodiment, catalyst libraries may be screened for both activity and
selectivity by high throughput screening using mass spectrometry. Catalyst libraries of
25 microreactors and direct transfer of reaction products to a mass spectrometer for analysis
according to this invention provides rapid screening of catalyst libraries. The technique
15 and apparatus of this invention using catalyst libraries of an array of microreactors in
monolithic structures with free jet sampling probes passing reaction products to a mass
spectrometer makes it possible to screen each site in about one to five seconds, a
30 significant improvement over the teachings of the Cong, et al reference cited above,
while eliminating potential wall effects inherent in capillary microprobe sampling.

20 In another embodiment, the mass spectrometric analysis may also be used in
35 combination with resonance-enhanced ionization of product gases and microelectrode
screening. In cases where both screening methods are feasible, radiation activation may
be used to rapidly identify promising sites and then mass spectrometry may be used to
40 quantify yields and selectivities in greater detail. In instances in which the identification
25 of radiation frequencies over which unique resonance enhanced multiphoton ionization
signals of reaction products may not be feasible, the mass spectrometric method may be
used to rapidly screen catalyst libraries.

45 Detection methods in situ in the reactor use the high sensitivity, specificity and
real-time features of resonance-enhanced multiphoton ionization, REMPI, in which
30 pulsed and tunable ionizing light sources are used to selectively photoionize desired
reaction products without ionizing reactants and/or other background species.

50 Photoions or photoelectrons generated by a tunable light beam in a reaction product

5 plume from reactants in contact with a specific catalyst library site are detected by an
array of microelectrodes positioned in close proximity to the library sites. While this
invention will be described using a tunable ionizing beam, any radiation beam of an
10 energy level to promote formation of specified photoions and photoelectrons may be
15 used. When reaction products are solids or liquids, they can be ablated using a pulsed
laser beam followed by selective photoionization of the products using a suitable UV
laser. The process of this invention can provide information on catalyst selectivity by
detecting several reaction product species. This can be done using different light
15 frequencies to sequentially generate specific ions of different products and the REMPI
10 signals can then be converted into absolute concentrations by use of calibration
20 standards.

Internal calibration standards introduced with the reactant feed can be used to
quantify reaction products, as will be readily apparent to one skilled in the art. The
process of this invention is broadly applicable and can be used to simultaneously screen
25 an entire catalyst library. The process of this invention can also be used to study
15 operational lifetimes, resistance to poisoning, regeneration and loss of catalysts in tests
or in full scale chemical plant processes.

30 The process of this invention for rapid screening of potential catalyst libraries for
catalytic properties broadly comprises; forming a potential catalyst library having
20 potential catalysts at a plurality of addressable sites, passing reactant gas in contact with
the potential catalysts at the plurality of addressable sites, and screening gas plumes of
35 products of reaction from the addressable sites, the screening comprising at least one of
translating one of the addressable sites into a position in proximity to a sampling probe
orifice followed by passing products of reaction through a free jet sampling probe to a
40 mass spectrometer for analysis and passing a radiation beam of an energy level to
promote formation of specified ions and electrons in the product stream, such as, for
example, a laser beam of a frequency to promote formation of specified photoions or
45 photoelectrons and detecting the formed photoions or photoelectrons by microelectrode
collection in situ in proximity to the addressable sites.

30 The above advantages and other features of this invention will be better
understood upon reading specific embodiments of the invention with reference to the
50 figures wherein:

5 Fig. 1 is a schematic showing the principles of REMPI microelectrode detection
of product species;

10 Fig. 2 is a schematic showing REMPI microelectrode detection of products
formed by reactant contact of a catalyst library with physical masking;

15 Fig. 3 is a schematic showing REMPI microelectrode detection of products
formed by reactant contact of a catalyst library through a dedicated reactant feed tube;

20 Fig. 4 is a schematic showing similar to Fig. 3 having a tilted test site;

25 Fig. 5 is a schematic showing REMPI microelectrode detection of products
formed by reactant contact of a catalyst library with flow through porous sites;

30 Fig. 6 is a schematic showing REMPI microelectrode detection of products
formed by reactant contact of a catalyst library of catalyst coating on a monolithic
structure;

35 Fig. 7 is a schematic showing of a monolithic catalyst library with expansion
cooling of products for REMPI microelectrode detection;

40 Fig. 8 is a schematic showing of a reactor with a flat plate solid catalyst library
with row REMPI microelectrode detection;

45 Fig. 9 is a schematic showing of a reactor with a flat plate catalyst library having
reactant flow through porous sites and row REMPI microelectrode detection;

50 Fig. 10 is a schematic top view of a reactor as shown in Fig. 9 having
simultaneous REMPI detection of all sites;

55 Fig. 11 is a schematic showing of a reactor with a monolith solid catalyst library
having reactant flow through with row REMPI microelectrode detection;

60 Fig. 12 is a schematic showing of a reactor with a monolith catalyst library having
simultaneous REMPI detection of all sites;

65 Fig. 13 is a schematic showing of a catalyst library with reactant contact for
homogeneous catalyst sites with REMPI microelectrode detection of products;

70 Fig. 14 is a schematic showing of a reactor with a homogeneous catalyst library
with reactant flow through with row REMPI microelectrode detection of products;

75 Fig. 15 is a schematic showing of a catalyst library using solid catalyst particles
for gas distribution and for catalyst contact with REMPI microelectrode detection of
products;

80 Fig. 16 is a schematic showing of a heterogeneous catalyst library with reactant

5 flow through with expansion cooling of products for REMPI microelectrode detection;

10 Fig. 17 is a schematic showing of a catalyst library using an ablation laser for gasification of solid and/or liquid products for REMPI microelectrode detection of products;

15 5 Fig. 18 is a molecular beam REMPI spectra for benzene and cyclohexane by TOF-MS;

20 Fig. 19 is a microelectrode REMPI spectra for benzene and cyclohexane;

25 Fig. 20 is microelectrode REMPI signals from screening of catalyst library site activity for benzene production.

30 10 Fig. 21 is a schematic showing of one embodiment of a single microreactor system of this invention;

35 Fig. 22 is a schematic showing of another embodiment of a single microreactor system of this invention suitable for solution deposition;

40 15 Fig. 23 is a schematic showing of an array of microreactors in a single body;

45 Fig. 24 is a schematic showing of another embodiment of an array of microreactors in a single body with a cover wafer;

50 20 Fig. 25 is a schematic showing of a catalyst library in vertical stacked arrays of microreactors as shown in Fig. 24;

55 Fig. 26 is a schematic showing a microreactor array as shown in Fig. 24 fitting into a frame;

60 25 Fig. 27 is a schematic showing of arrays of microreactors in frames as shown in Fig. 26 arranged in adjacent side-by-side configuration;

65 Fig. 28A and 28B are diagrams summarizing combinatorial catalyst library preparation and screening according to one embodiment of this invention;

70 30 Fig. 29 is a cross sectional schematic showing of a sampling probe having a conical orifice in sampling mode for transfer of reaction products of one site in a catalyst library in an array of microreactors to a mass spectrometer for analysis;

75 35 Fig. 30 is a schematic showing of a sampling probe similar to Fig. 29 having a capillary orifice in a translation mode;

80 40 Fig. 31 is a perspective schematic showing of an array of microreactors with a sampling probe for passage of a portion of reaction products to a mass spectrometer in combination with an activating energy beam for REMPI measurement on a translation

5 table for translation in a single dimension; and

10 Fig. 32 is a perspective schematic showing of horizontally stacked arrays of
microreactors on a translation table for translation in two dimensions for combined mass
spectrometer and REMPI measurement of reaction products from a catalyst library.

15 5 Generation of combinatorial solid state libraries has been achieved by sputtering
with physical masking for measurement of superconducting, Xiang, et al, 1995, *supra*,
magnetoresistivity, Briceno, et al, 1995, *supra*, and luminescence, Wang, et al, 1998,
supra and Sun, et al, 1997, *supra*. Other thin film deposition techniques are known to
the art, such as, electron beam evaporation, Danielson, et al, 1997, *supra*, thermal,
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Supported Molybdenum Carbide Catalyst", *Chem. Lett.*, 121, 561, 1996, and plasma,
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Fe₃O₄(001) Films by Plasma-Assisted Molecular Beam Epitaxy, *Surf. Sci.*, 371, 358,
1997, and pulsed-laser deposition, Gorbunov, A.A., Pompe, W., Sewing, A., Gapanov,
30 35 S.V., Akhsakhalyan, A.D., Zabrodin, I.G., Kaskov, I.A., Klyenkov, E.B., Mozorov,
A.P., Salaschenko, N.N., Dietsch, R., Mai, H. and Vollmar, S., "Ultrathin Film
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649, 1996 and Russo, R.E., Mao, X.L. and Perry, D.L., "Make Catalytic Coatings by
35 40 Pulsed-Laser Deposition", *Chemtech*, 12, 14, 1994, can be used to create large solid
state catalyst libraries. These techniques provide good control of surface chemistry and
are ideally suited to generate a wide spectrum of solid materials. Other well established
40 45 preparation techniques, such as co-precipitation and impregnation, can also be used to
generate catalyst libraries. Satterfield, C.N., "Heterogeneous Catalysts in Practice", 2nd
Ed., Chap. 4, 87, McGraw Hill, New York, 1991. For example, a large variety of co-
precipitates can be synthesized in parallel and the resulting slurries/pastes can be applied
45 50 on suitable substrates using, for example, multichannel pipettes or solenoid inkjet valves
30 to generate spatially addressable sites. Lemmo, A.V., Fisher, J.T., Geysen, H.M. and
Rose, D.J., "Characterization of an Inkjet Chemical Microdispenser for Combinatorial
Library Synthesis", *Anal. Chem.*, 69, 543, 1997. Catalyst libraries can also be prepared

5 by impregnating suitable carrier materials, such as, for example, porous silica or alumina, that were previously applied to addressable sites on a substrate by a suitable liquid solution containing a catalyst. The slurries/pastes and impregnation solutions applied on the substrates can then be dried and treated to produce suitable catalyst materials.

10 5 Porous catalyst libraries can also be prepared by coating porous carriers, for example, silica or alumina, with thin films of catalytic materials using various film deposition techniques described above. An important aspect of this approach is prevention of excessive deposition to prevent pores becoming plugged by the catalytic materials. Reactant contact with the porous libraries can be accomplished either by passing

15 10 reactants over or through the catalyst sites.

20 In testing for catalysis, however, chemical composition is not the sole determinator of activity. Physical properties of the surface, such as edges, corners and defects, as well as pore size can have an influence in determining activity. Satterfield, C.N., 1991, *supra* and Smith, J.M., "Chemical Engineering Kinetics", Chap. 8, 327-358,

25 15 McGraw Hill, New York, 1981. These properties are determined to a large extent by the catalyst preparation procedure. Therefore, thin film combinatorial libraries may be subjected to a variety of treatment methods to generate suitable catalytic materials, such as, for example, oxidation, reduction, calcination, leaching, the subsequent addition of dopants and other treatments well known to the art. These different preparation

30 20 processes also substantially increase the number of combinations of catalyst formulations which must be tested in order to obtain the best catalyst.

35 Heterogeneous catalyst libraries can also be prepared by using monolithic, or honeycomb, structures. Satterfield, C. N., 1991, *supra*. These materials provide parallel, uniform, straight and nonconnecting channels, thereby providing a convenient matrix for creating large catalyst libraries. A variety of cell shapes and sizes with cell densities varying from about 10 to about 500 cells per square inch can be produced with catalyst library sites. However, a wide variety of desired custom cell densities can be fabricated within and beyond the above ranges. Monolithic structures can be made from metals or 40 25 they can be extruded from inorganic dough, such as magnesia-alumina silicate, through a die followed by drying and firing. Catalyst libraries can also be prepared by coating

45 30 metal monoliths with inorganic substrates, wherein the metal inlay serves as a barrier to prevent intercell diffusion of species. Catalysts can then be incorporated into the library

5 substrate using any of the variety of methods described above. Monolith structures can also be machined for optical access and placement of microelectrodes.

10 Homogeneous catalyst libraries comprising, for example, organometallic and inorganometallic compounds and other complex molecules such as enzymes, can be 10 similarly generated using multichannel pipettes, Burgess, K., Lim H-J., Porte, A.M. and Sulikowski, G.A., "New Catalyst and Conditions for a C-H Insertion Reaction Identified by High Throughput Catalyst Screening", *Angew. Chem. Int. Ed. Engl.*, 5, 220, 1996, 15 and solenoid inkjet valves. These libraries may have arrays of microtubes bundled together with reactant gas bubbled through them. Homogeneous liquid catalysts can also 20 be held or immobilized in the pores of porous carriers which can be in the form of particles or can be coated on the walls of monolithic structures. Since the screening method of this invention can be readily miniaturized, the physical dimensions of catalyst 25 sites that determine library density are primarily dependent upon the nature of the catalyst, liquid or solid phase, the method of preparation of the library, diffusional mixing 30 of gases in the library, heat conduction through the library substrate, the objectives of the screening process and other relevant factors. For example, when the objective of screening is to evaluate catalytic materials for gas-phase reactions using flat catalytic 35 sites, library densities will be limited by the gas-phase diffusion because at high library densities intersite diffusion can result in signal crossovers between sites. However, the 40 evaluation of catalyst operating temperature windows requires the fabrication of libraries in which each site is thermally insulated to maintain different temperatures. In this case, the library density will be limited by the thermal conductivity of the wafer of substrate. For liquid phase homogeneous catalysts, surface tension and viscosity play a significant 45 role in determining gas dispersion, and thus in establishing the minimum dimensions of 50 the library sites and hence the library density.

In this invention, the catalyst sites must be sufficiently separated from each other so that product formation from each site and its unambiguous detection can be achieved. Monolithic, or honeycomb, structures offer advantages by providing clear physical separation of the library sites. These and other catalyst library design factors will be 45 further discussed in descriptions of screening methods. Unambiguous and rapid 50 screening of solid catalyst sites of 0.5 cm by 0.5 cm have been demonstrated using the present invention. These site dimensions provide catalyst libraries having densities of

5 about 10 sites per square inch which permits creation of over 900 sites on a substrate
10 having dimensions of 8.5 inches by 11 inches, the size of a sheet of letter paper. Higher
15 library densities are clearly practical using smaller site dimensions or by the use of
monolithic structures. The pattern of the sites should be designed to expedite the
20 generation and screening of the libraries, libraries having rows of catalyst sites offering
distinct advantages both for generation and screening of the sites. Any method of
25 production of chemical libraries having sites of the above mentioned characteristics is
suitable for production of catalyst libraries for use in the rapid screening process for
30 catalyst evaluation according to this invention.

35 10 In one embodiment of this invention, sampling of reaction products emanating
from individual sites in a library is accomplished by passing the reaction products through
40 a small orifice, placed in close relationship to the source of the reaction products, to a
significantly larger cross section area chamber for passage to a detection device, such as,
45 a mass spectrometer. Shown schematically in Fig. 29 is a catalyst library having
50 individual sites configured in microreactors, as will be described below in further detail.
Briefly, inert microreactor body 100 has reactant feed passages 102 leading to enlarged
55 catalyst zones with catalyst beds 101. Reactant gases are supplied through reactant gas
supply passage 103 to reactant gas distribution plenum 104 for distribution to reactant
60 feed passages 102. Reaction products exit the microreactors through reaction products
65 exit passages 105 and pass from reactor enclosure 106 or a portion may pass from an
70 individual library site through a micro sampling probe to a detection device. The reactor
75 enclosure can be pressurised to provide the desired reaction pressure. Alternatively,
80 each microreactor can be individually pressurised to test catalysts under different
85 pressures, or each array of microreactors can be individually pressurised. As shown in
90 Fig. 29, the catalyst library is fixidly mounted on translation table 107 for positioning of
95 sampling probe 108 over a single library site for detection of reaction products from that
site. Translation table 107 may be moved in x-y-z directions by computer controlled
100 stepper motors, as well known by one skilled in the art, to rapidly move single library
sites into position for sampling from a single site by sampling probe 108 fixidly mounted
105 in reactor enclosure 106. It is also possible to translate the sampling probe and the
110 detection system while maintaining the library stationary, or both the library and the
115 sampling probe may be simultaneously moved by translators. As shown in Fig. 29, a

5 single library site has been moved to a sampling position in proximity to sampling probe
10 108 to pass a portion of reaction product gases through the sampling probe to mass
spectrometer 109. Reactants may be passed through all library sites may be operated
15 simultaneously and product gases from other library sites may be withdrawn from reactor
10 enclosure 106. Following product gas analysis at a particular library site, the library may
be translated into position for evaluation of another catalyst site. Since several or all of
15 the sites in a library may be under reaction conditions simultaneously, analysis of the
reaction products may take place immediately after positioning the library without the
necessity of waiting for equilibrium conditions and without transfer line delays
10 encountered by use of capillary tube sampling probes, as described by Cong, et al, supra.
20 The tip of sampling probe 108 must be made from material which can be
machined and withstand the pressure and temperature of the reaction chamber, in the
event that the reactor enclosure 106 is pressurised, as well as being inert to the reactants
25 and reaction products. As shown in Fig. 29, reactor enclosure wall 106 has sampling
15 cone 110 which may be integral with or attached with proper sealing to the reactor
enclosure wall. When the microreactors in the reactor array are internally pressurised
and products discharged into atmospheric pressure, the sampling cone can be directly
30 attached to the mass spectrometer. As shown, sampling cone 110 has a sampling probe
extension 111 to minimally perturb the reaction product stream and allow positioning of
20 the sampling probe very close to the catalyst reaction site without hindering product gas
venting. Sampling cone 110 should have a half cone angle of about 15 to about 45
35 degrees to allow free jet expansion of the gas samples into a vacuum chamber while
sampling probe extension 111 may have a smaller cone angle. Free jet expansion in the
sampling probe leads to substantial cooling and quenching of all possible homogeneous
40 and heterogeneous reactions and provides direction to the molecules towards a mass
spectrometer positioned downstream of the sampling cone. Sampling cone orifice 112,
45 at the small end of the cone, is sized so that reaction chamber pressures and vacuum
pump capacities of all stages can be accommodated. Suitable sampling cone orifice
diameters are about 1 micrometer to about 200 micrometers, typically about 5
50 micrometers to about 50 micrometers for use with modest size vacuum pumps. The
expanding reaction product sample from the sampling cone passes through first vacuum
stage 113 and skimming cone 114 to ensure that only the central portion of the reaction

5 product sample jet enters the mass spectrometer chamber, eliminating any surface
induced reactions that may occur in the sampling probe. The cone angle and diameter of
the opening at the tip of the skimmer must be suitable to meet reaction chamber pressure
and sampling probe pumping speed requirements, as can be readily determined by one
10 skilled in the art. The reaction product sample jet passing through the skimming cone
then passes through second vacuum stage 115 and is directly introduced into a mass
spectrometer through mass spectrometer inlet orifice 116. The mass spectrometer can
be a quadrupole mass spectrometer or a time of flight spectrometer with fast electronics
15 to acquire and process the data, as well known to the art. Electron impact or radiation
10 can be used to ionize species. Tunable lasers can also be used to selectively ionize
reaction products under REMPI conditions. When catalyst libraries are screened at
20 atmospheric pressure, or when microreactor arrays are internally pressurised and
products discharged to atmospheric pressure, only one pump down stage may be
necessary to prepare the sample for mass spectrometer pressure conditions, while
25 catalyst libraries screened at high pressures may require more than two pump down
stages, as will be apparent to one skilled in the art. The staged pump down process
rapidly brings the pressure of the reaction products from high pressures, in some
30 applications from about 20 to about 50 atmospheres, to a small fraction of an
atmosphere so that the reaction product samples can be directly introduced into the mass
spectrometer where pressures are typically maintained at about 10^{-5} to about 10^{-6} Torr.
35 When microreactors in an array are internally pressurised and discharged into
atmospheric pressure, this will constitute a pump down stage. The pressure of the last
pump down stage, second stage in Fig. 29, and the mass spectrometer inlet orifice
40 diameter must be compatible with this pressure limitation in view of the pumping speed
attainable by the vacuum system. Typically, pressure in the first and second stages of a
two stage system should be maintained at about 760 to about 10^{-2} and 10^{-2} to about 10^{-5}
45 Torr, respectively. The pressures in all stages should be maintained the same during
calibration and screening processes to quantify the results of catalyst evaluation.
The distance from the sampling probe orifice to the mass spectrometer should be
50 kept as short as possible to maximize detection sensitivity since the gas concentration
decreases upon expansion into vacuum according to $1/r^2$, where r is the distance from the
tip of the sampling probe. However, shorter sampling probe orifice to mass

5 spectrometer distance decreases the pumping speed provided by the vacuum pump(s),
thereby adversely affecting the free jet sampling process. In view of these conflicting
10 results, the spacing between the sampling probe orifice and the mass spectrometer is
determined to balance signal detection and pumping speed needs. Typically, spacing
15 5 between the sampling probe orifice and the mass spectrometer is about 7.5 to about 25
cm. In the limit, the sampling system performance approaches molecular beam
sampling conditions as described by Chang, W.D.; Karra, S.B.; and Senkan, S.M.,
Molecular Beam Mass Spectroscopic Study of Trichloroethylene Flames, Environ. Sci.
Technol., 20, 12, 1243, (1986) where the expanding sample jet velocities in the first
20 10 stage can reach supersonic levels and the jet stream entering the mass spectrometer is a
directed molecular beam.

Another embodiment of the invention is shown in Fig. 30 wherein the
25 microreactor array catalyst library is shown in translation mode withdrawn from the
sampling position shown in Fig. 29 and sampling orifice 117 is a short capillary inert to
15 reactants and reaction products having a diameter of about 1 to about 500 micrometers,
typically about 5 to about 100 micrometers, and lengths of about 1 micrometer to about
20cm, typically about 5 to about 100 micrometers. The capillary orifice used in this
30 invention is significantly shorter than those used by Kassern, M., Qum, M., and Senkan,
S. M., *supra*, and by Cong, P., Giaquinta, D., Guan, S., McFarland, E., Self, K., Turner,
20 H. and Weinberg, W.H., *supra*. To maximize product sample signals and to minimize
pumping speed requirements, capillary diameters of about 5 to about 20 micrometers and
35 capillary lengths of about 50 to about 100 micrometers are compatible with small
commercial vacuum pumps. The capillary orifice of this embodiment passes directly into
first vacuum stage 113 of sampling microprobe 108. In other respects, the apparatus and
40 25 process shown in Fig. 30 is similar to those described above with respect to Fig. 29.

In the sampling probe configurations shown in Figs. 29 and 30, the time required
45 to transfer reaction products from the reaction zones of the microreactors to the mass
spectrometer can be in the order of microseconds to tens of milliseconds. Acquisition of
mass spectrometric data can be accomplished in a time scale of the order of several
50 30 hundred milliseconds, especially when specific mass ions are monitored. Therefore, the
time limiting step of the screening process is the time to mechanically position individual
sites in the library in sampling position, in proximity to the sampling orifice of the

5 sampling probe, by the stepper motor driven translation apparatus. All microreactor sites
10 in the catalyst library can be simultaneously operated to simultaneously generate reaction
products. In this mode, the product stream from any site in the library can be sampled at
15 any time without the requirement of waiting for establishment of steady state operating
5 conditions in each site. Alternatively, reactant gas flows to individual sites in a library
may be independently controlled by flow controllers in each reactant feed passage so that
reactant flow to a specific library can be turned on early enough for establishment of
10 steady state operating conditions while screening another site and then turned off after
the screening process of that site, as more fully explained below. This mode of operation
20 is necessary when it is important to screen the library sites at the same on-stream time
conditions.

The catalyst library shown in Figs. 29 and 30 represent a cross section of an array
of packed bed microreactors in a high thermal conductivity metal microreactor body.

Catalyst powders, particles, or any other form of solid catalysts, can be placed into
25 cylindrical, or other shaped, cartridges which can be inserted into the catalyst zones of
15 the microreactor body. Other methods of catalyst loading of microreactors, as more
fully explained below, are also suitable. Reactor heating elements 118 are shown
30 embedded in microreactor body 100 to provide uniform temperature control of the entire
library. Individual library sites also may be insulated from each other and each have an
20 individually controlled heating element to provide different temperature control of each
site. In a similar manner, each site may be provided with an individual flow control
35 regulator to provide different residence times in each site. A similar reactant preheat
zone in the reactant feed zone may be provided, as shown by reactant preheating
20 elements 119, to heat reactant gases to a desired temperature prior to contact with the
catalyst. These microreactor configurations are more fully described below. The entire
40 library is attached to translation table 107 in a fixed relation to provide precision x-y-z
three dimensional movement, as indicated by translation arrows 120. Two dimensional
45 translation in the x and y axes moves the library into position for sampling a specific site
while movement in the third dimensional z axis positions reaction product exit passage
30 121 into proximity to sampling cone orifice 112 of sampling microprobe 108.

50 The mass spectrometric screening method described above can be used with
other catalyst library designs, such as, for example, those described herein as well as

5 other types of libraries which may include homogeneous catalyst libraries, fluidized bed
10 (gas and liquid) libraries, and combinations thereof. The mass spectrometric screening
method may be combined with the resonance-enhanced multiphoton ionization method,
REMPI, described in greater detail herein. The REMPI method for screening catalyst
15 libraries has been more fully described in Senkan, S.M.; High-Throughput Screening of
Solid-State Catalyst Libraries, *Nature*, 394, 350, 23 July 1998. The combination of mass
spectrometric screening, as described above, with a microreactor array as shown in and
described further in respect to Fig. 24 is shown in Fig. 31. As shown in Fig. 31,
20 microreactor array 122 has activating radiation beam 77 passing through the reaction
product streams from the individual sites with microelectrodes 87 in proximity thereto
with internal wiring leads 88 for powering each electrode and for passage of detection
signals from each electrode to a detection device. In the manner as described above with
respect to Fig. 29, sampling cone tip 111 with a sampling orifice is placed in proximity to
25 the reaction product stream at the exit of an individual microreactor by movement of the
microreactor array on translation table 107 in an x direction and placed in sampling
15 position by movement of the microreactor array in a z direction, as indicated by
translation arrows 120.

30 Stacked arrays of microreactors for combined mass spectrometric and REMPI
screening methods may be formed using multiple microreactor arrays, as more fully
20 shown in and described with respect to Fig. 25. As in the case of reactor arrays shown in
Figs 29 and 30, heating elements can be embedded in thermal conducting walls between
35 individual microreactors. In similar manner as shown and described with respect to Fig.
31, REMPI measurements and/or mass spectrometric measurements may be made by
positioning the arrays to a single site for mass spectrometric sampling by movement of
40 translation table in the x-y-z axes indicated by translation arrows 120. Fiber optics
facilitates mounting laser light sources on translation table 107 to provide laser beams 77
to all of the library sites simultaneously for rapid REMPI microelectrode screening. In
45 cases where both methods of screening are feasible, radiation activation may be used to
rapidly identify promising sites and mass spectrometric analysis used to quantify yields
30 and activities more precisely.

50 It will be apparent to one skilled in the art upon reading of this description that
any of the microreactor configurations, microreactor arrays, and stacked arrays of

microreactors disclosed with respect to the REMPI microelectr de screening method may be readily adapted to the mass spectrometric screening method by mounting the microreactors on a suitable translation table and provision of a free jet expansion sampling probe leading to a mass spectrometer.

5 Screening of large libraries for desired catalytic activity according to this
invention is based upon the fact that when a laser frequency is tuned to a real electronic
intermediate state of a gaseous molecule, the cross section for ionization of that molecule
is significantly enhanced. This process is resonance-enhanced multiphoton ionization, or
REMPI. When the laser wavelength is not tuned to a real electronic state, the probability
10 for photoionization is very small. Thus, the ionization cross section reflects the
absorption-excitation spectrum of the intermediate electronic state of the molecule.
Using REMPI, specific catalytic reaction products can be selectively ionized with high
efficiency using a suitable laser frequency, while avoiding the simultaneous
photoionization of reactants and/or background gases. While preferred embodiments of
15 this invention are described using laser beams, any radiation beam of a suitable energy
level to promote formation of specified ions and electrons from reaction products may be
used, thereby allowing detection of the formed ion and/or electrons by microelectrode
collection in downstream proximity to the radiation beam.

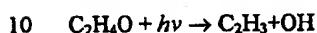
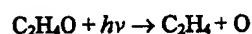
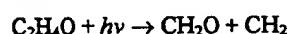
In cases where the catalytic reaction product(s) do not provide easy generation of REMPI photoions, the process of this invention may be used in detection of directly related products. For example, reaction product molecules may be fragmented into smaller daughter products by a suitable energy source, such as, for example, a pulsed laser beam or by a plasma arc. The fragments may be stable molecules, radicals or ionic species. Following fragmentation of a catalytic reaction product molecule to a daughter product which can be uniquely attributed to a catalytic reaction product molecule that is desired to be detected, the daughter product can be selectively photoionized using the REMPI process and detected by a microelectrode as described herein. Quantification of reaction products by detection of their fragmentation products requires additional calibration to account for the efficiencies of fragmentation.

30 It may also be possible that upon irradiation of reaction products by specific light frequency, the reaction products or their fragmentation products may emit unique radiation signatures involving, for example, luminescence, fluorescence or

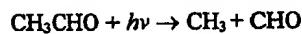
5 phosphorescence. These emissions can then be used to rapidly screen the catalyst
10 libraries using, for example, monochromators and diode array and charge coupled device
(CCD) detectors.

10 For example, selective identification of ethylene oxide (C_2H_4O) and acetaldehyde

15 (CH_3CHO) as a consequence of the reaction of ethylene (C_2H_4) and (O_2) can be
performed on fragmentation products which may be described by the following
equations:



20 In the case of acetaldehyde, the fragmentation may be described by the following:



25 Although it may be possible to detect the catalytic product molecules directly by
their REMPI ions, information about their presence in a reactant-product mixture can

30 15 also be obtained by measuring the REMPI characteristics of their fragmentation
products. Thus, the formation of fragmentation products CH_2O , CH_2 , C_2H_3 , O and OH
can be uniquely attributed to ethylene oxide while the formation of CH_3 and CHO can be
35 uniquely attributed to acetaldehyde. In this manner, the selective detection of any one of
the fragmentation products, except ethylene which is present abundantly as a reactant,
40 20 can signify the level of the parent ethylene oxide and/or acetaldehyde in a mixture of
these chemicals.

40 As another example, acrylonitrile (C_2H_3CN) when produced by the reaction of
propane (C_3H_8), ammonia (NH_3) and oxygen may be detected by detection of either of
45 the products resulting from the fragmentation $C_2H_3CN + h\nu \rightarrow C_2H_2 + CN$ which gives
25 unique information about the level of acrylonitrile in a product mixture.

50 45 There are several means for inducing REMPI, the most common is the resonant
2-photon ionization, R2PI, in which one photon, $h\nu_1$, energizes the molecule to an
excited electronic state and the second photon, $h\nu_2$, ionizes the molecule. Lubman, D.M.,
"Lasers and Mass Spectrometry", Oxford Univ. Press, New York, 1990, Chap. 16,
30 Lubman, D.M. and Li, L., "Resonant Two-Photon Ionization Spectroscopy of Biological
Molecules in Supersonic Jets Volatilized by Pulsed Laser Desorption", 353. However,
50 depending upon circumstances, the absorption of two or more photons in each step can

5 also be used for REMPI. Ionization occurs if $(hv_1 + hv_2) > IP$, where IP is the ionization potential. The two photons used can have the same or different energies and can be obtained from the same or different lasers. Higher energy UV photons may also be used to photoionize species in a single photon process. The two photon REMPI process can
10 5 be described for selective photoionization of a product P by the following equations: $P + hv_1 = P^*$ and $P^* + hv_2 = P^+ + e$, wherein P is the product, P^* is the real electronic excited state of the product, P^+ is the photoion of the product and e is the photoelectron. By
15 varying the photon energies, which can be accomplished using tunable lasers, the ionization spectrum of the target molecule P can be mapped to determine a suitable laser
20 10 frequency which can be used to exclusively ionize it without simultaneously ionizing other molecules in the mixture. Since the REMPI process involves the participation of two or more photons, the laser light wavelengths used must take this into account. As a crude approximation, each photon in a successful REMPI must possess an energy of about 1/2 the IP in the R2PI process using a single laser beam. Similarly, if a single laser
25 15 beam is used, each photon energy must be about 1/3 the IP in a 2 + 1 process and 1/4 the IP in a 2 + 2 process, etc. When two or more laser beams are used, each photon energy can be independently selected to optimize the resulting REMPI signals. Laser
30 30 wavelengths covering the range from deep ultraviolet, UV, such as 150 nanometers, nm, to visible light, such as 700 nm, can be used to induce REMPI using a variety of
20 multiphoton processes.

35 REMPI is inherently a high resolution technique in which ion absorption features of any molecule can be determined with high precision. Also, molecules are ionized from a vibrational level of an electronically excited state, thereby providing specific photoionization of only target molecules. This can be used to distinguish between
40 25 isomers, for example dichlorotoluenes, due to their different electronic structures. Zimmerman, R., Lerner, Ch., Schramm, K.W., Kettrup, A. and Boesl, U., "Three-dimensional Trace Analysis: Combination of Gas Chromatography, Supersonic Beam UV Spectroscopy and Time-of-Flight Mass Spectrometry", Euro. Mass Spectrom., 1, 341, 1995. The REMPI process can be sequentially used to detect different products
45 30 using different laser frequencies, thus also providing the determination of catalyst selectivities. REMPI is a high sensitivity technique with real-time detection of species at low parts per billion, Gittins, C.M., Castaldi, M.J., Senkan, S.M. and Rohlfing, E.A.,

5 "Real-Time Quantitative Analysis of Combustion Generated Polycyclic Aromatic
10 Hydrocarbons by Resonance Enhanced Multiphoton Ionization Time of Flight Mass
Spectrometry", Anal. Chem., 69, 287, 1997, and high parts per trillion already
demonstrated. Castaldi, M.J. and Senkan, S.M., "Real-time Ultrasensitive Monitoring of
15 5 Air Toxics by Laser Photoionization Time of Flight Mass Spectrometry, J. Air and
Waste Mgmt. Assoc., 48, 77, 1998.

10 Fig. 1 is a generalized illustration of the REMPI method of selective detection of
a gaseous product generated by contacting a catalytic site with reactants. According to
the present invention, gaseous reaction products form a gaseous plume 22 when catalyst
15 10 mounted on substrate 20 is contacted by the reactants. The gaseous products are
photoionized by pulsed UV laser beam 23 formed from tunable laser source 24 and/or
20 using second tunable laser source 25 directed by mirror 26 through the central portion of
gaseous product plume 22 generating photoions, P^+ , and photoelectrons e^- , as indicated
25 in Fig. 1. Microelectrode 27 is positioned a few millimeters above laser beam 23 to
15 collect the photoelectrons or photoions, depending upon the voltage bias applied by DC
power source 30 to cathode 28 and anode 29. The electrical signal collected by
30 microelectrode 27 is then amplified and detected by detector 31, such as a digital
oscilloscope. If the measured electrical signal is higher than reference sites which do not
have catalysts, the site can be tagged catalytically active. Otherwise, the site must be
20 considered catalytically inactive. It is apparent that selection of a suitable laser
frequency, or frequencies for detection of multiple products, is critical to ensure that the
35 electrical signals generated by the laser beam are exclusively due to photoionization of
the specified product gas and not from the reactants and/or background gases. The
suitable laser frequency for a specific material may be identified by laser photoionization
40 mass spectrometry studies, using for example, a tunable laser and time-of-flight mass
spectrometer. Castaldi, M.J. and Senkan, S.M., 1997, *supra* and Gittins, C.M., Castaldi,
M.J., Senkan, S.M. and Rohlfing E.A., 1998, *supra*. Using this approach, a gas mixture
45 containing the species of interest is introduced into a vacuum chamber using, for
example, a pulse valve. The expanding gas jet is then intercepted by UV photons at a
30 specific energy from a tunable laser generator. The resulting REMPI signals are then
recorded by the time-of-flight mass spectrometer system. By scanning the UV laser
frequency range, the photoionization spectra of the reactants, products, by-products and
50

5 background gases can be determined. In the case of molecular isomers, the
10 photoionization spectra of each isomer must be determined individually. Following the
determination of the photoionization spectra for all of the relevant species, specific UV
15 frequencies can be identified which would lead to the exclusive generation of the REMPI
ions of specific product isomers desired to be evaluated.

5 It should be recognized that the REMPI spectra broadens at elevated
10 temperatures due to the overlapping transitions from a large number of rovibronic levels.
15 However, it is generally possible to identify a laser frequency that selectively
photoionizes the desired products without interferences from the reactants, other
20 products and the carrier gas, due to the availability of broadly tunable UV lasers. This
identification process is expedited when the product gases are structurally different from
the reactant and background gases, for example, in the production of benzene, an
25 aromatic compound, from hexane, an aliphatic compound, in Ar carrier gas with H₂ as
the only by-product. Potential problems associated with spectral congestion of REMPI
30 signals can be effectively solved by the use of supersonic jet expansion. Parker, D.H.,
"Laser Ionization Spectrometry and Mass Spectrometry" in "Ultrasensitive Laser
Spectroscopy" Kliger, D.S. Ed., Academic Press, New York, 1983 and Trembleau, R.,
35 Sin, C.H., Li, P., Pang, H.M. and Lubman, D.M., "Applicability of Resonant Two-
Photon Ionization in Supersonic Beam Mass Spectrometry to Halogenated Aromatic
40 Hydrocarbons", Anal. Chem., 57, 1186, 1985. Jet expansion, which can be achieved by
expanding the product gases into a vacuum through a small orifice, leads to transitional,
45 rotational and vibrational cooling resulting in significant simplification of the REMPI
spectra. This method permits selective detection of specific species in a similar
background.

40 The product photoions and photoelectrons generated above the catalyst site can
be collected using a microelectrode, which can be either anode or cathode or both. The
substrate upon which the catalyst library is deposited can also serve as the cathode or the
anode, or another microelectrode can be placed within the substrate for this purpose.
45 High temperature REMPI-electrode approach has previously been used to determine the
30 concentration of gaseous species containing only a few atoms, such as PO, NO, H and
O. Smyth, K.C. and Mallard, W.G., "Two Photon Ionization Processes of PO in a
50 C₂H₂/air Flame", J. Chem. Phys., 77, 1779, 1982; Cool, T.A., "Quantitative

5 Measurement of NO Density by Resonance Three-Proton Ionization", App. Optics, 23,
10, 1559, 1984; Goldsmith, J.E.M., "Resonant Multiphoton Optogalvanic Detection of
Atomic Oxygen in Flames", J. Chem. Phys., 78(3), 1610, 1983; and Bjorklund, G.C.,
15 Freeman, R.R. and Storz, R.H., "Selective Excitation of Rydberg Levels in Atomic
5 Hydrogen by Three Photon Absorption", Optics Comm., 31(1), 47, 1979. These earlier
studies, which exhibit problems of spectral congestion and broadening of REMPI signals,
15 implicitly teach against use of the REMPI-electrode approach when larger molecule
species are involved. However, it has now been discovered that larger molecules can be
10 measured by this technique for catalyst screening. Significant broadening of the REMPI
spectra can be tolerated in catalyst screening where the REMPI features of the reactants
20 and products are generally separated. When the REMPI spectra overlap, which should
be rare in catalyst screening where reactants and products have distinct electronic
structures, this problem can be solved by jet cooling the products by expanding them into
a vacuum chamber through small orifices.

25 15 The REMPI microelectrode technique can also be used to detect liquid and solid
products. In these cases, the reaction products must be gasified first using an ablation
30 laser, for example, a pulsed CO₂ or another type of laser. The gasified products then can
be photoionized by REMPI and detected by a microelectrode, as described above. The
35 REMPI method can also be used to monitor reaction intermediates involved in the
20 catalytic process, which cannot be detected by analysis of product gases collected at the
exit of the reactor. This can be particularly useful in developing insights into reaction
pathways associated with catalytic reactions, and thereby can significantly accelerate the
catalyst development process

40 No literature is known to the inventor which suggests the use of REMPI and
25 microelectrodes for the high speed screening of heterogeneous and homogeneous
catalyst libraries. A multitude of approaches for the rapid screening of large libraries for
45 catalytic activity may be followed, and the following presently preferred approaches are
set forth as exemplary and should not be considered as limiting the invention.

30 For heterogeneous catalyst libraries, the solid state catalysts may be arranged in
rows of catalyst clusters on a flat sheet to expedite the screening process. In addition,
50 monolithic, or honeycomb, structures with well defined channels can also be used to
generate suitable catalyst libraries. The catalyst sites can also be created to be porous or

5 non-porous depending upon the catalyst and method of preparation. Fig. 2 illustrates a
10 non-porous, flat sheet catalyst library with reactant contact with the catalyst achieved by
flowing reactant gases over the library followed by row screening of product plumes.
15 The same numerals have the same meaning throughout this disclosure and in the figures.
5 Test catalyst site 21 with upstream catalyst site 21u and downstream catalyst site 21d are
shown on substrate 20 with mask 32 shielding upstream catalyst site 21u from the
reactant gas stream indicated by reactant velocity profile 33. The gases containing
products must be removed from the library after their emanation from the sites to
minimize product circulation in the reactor. In the arrangement shown in Fig. 2, the
10 catalyst sites upstream from the test catalyst site, 21, must be masked to prevent signal
crossover from different sites. If the upstream sites are not masked and if some of these
sites are catalytic, products formed at these sites would be transported downstream and
interfere with the row screening process. Masking can be accomplished by using a
25 physical mask to cover upstream catalyst sites, as shown in Fig. 2, or by introducing
15 reactant gases directly onto the catalyst sites using dedicated gas reactant feed tubes,
shown as 34 in Fig. 3. Fig. 4 shows tilted catalyst test site 21t to promote transport of
products away from the catalyst surface. This arrangement improves signal detection of
30 products from the test site.

When reactant molecules pass over the test sites with catalytic properties,
20 products will be formed at the surface. These products will then diffuse into the flowing
gas stream and establish a product concentration boundary layer, or product plume 22,
35 as shown in Figs. 2-4. Assuming a constant catalyst surface concentration for the
product, the product concentration layer thickness $\delta_c(x) = 3.3(DxL/U_c)^{1/3}$, where x is the
distance from the leading edge of the catalyst site as shown in Figs. 2-4, D is the
40 molecular diffusion coefficient of the product, U_c is a characteristic gas velocity as shown
in Figs. 3-4 and L is a characteristic dimension in the vertical direction, such as the height
of the reactor or the diameter of the reactant feed tube shown in Figs. 3-4 as 2R.

To illustrate some of the design issues involved, consider the solid state library of
45 catalyst sites 5 mm long by 5 mm wide. Assuming a gas feed line diameter of 0.5 cm and
30 a mean reactant gas velocity of 1.0 cm/sec and a diffusion coefficient of 0.1 cm²/sec
which is typical for most gases at 1 atm, the concentration boundary layer thickness at 5
50 mm from the leading edge of the catalytic site can be estimated to be:

5

$$\delta(0.5) = 3.3[(0.1)(0.5)(0.25)/1.0]^{1/3} = 0.767\text{cm or }7.67\text{mm}$$

10

This boundary layer is thick enough to pass a laser beam through and to
5 photoionize products, if present. The diameter of the gas feed tube 2R, the gas velocity
U_o and the catalyst site dimension x can be altered to further control the thickness of the
15 concentration boundary layer. Additionally, test sites 21t can be tilted, as shown in Fig.
4, during the screening process to promote the transport of products away from the
catalyst surface.

20

When porous catalyst libraries are generated, reactant gases can also be passed
through the sites in the library generating a product plume above the test catalyst sites, as
shown in Fig. 5. In this embodiment, the reactants pass through all of the catalyst sites
thereby rendering simultaneous screening of all sites on the library feasible. As shown in
25 Fig. 5, reactants are passed through reactant plenum 36 to and through porous test sites
15 21p forming product plumes 35 which are measured in the same manner as described
above.

30

Catalyst libraries may also be created, as shown in Fig. 6, using monolithic
structures 40 wherein reactant gases will also pass through channels 37 over catalyst
coatings 38 forming product gases which pass through laser beam 23 and over
20 microelectrodes 27. In this embodiment, simultaneous screening of the entire library is
readily accomplished. Microelectrodes 27 may be inserted into channels 37, as shown in
35 Fig. 6, to significantly reduce signal crossover between catalytic sites. Optical access to
the product gases in each channel must be provided through small windows 39 for the
laser beam, as shown in Fig. 6. As a consequence of good spatial resolution and site
40 separation provided, monolith structures provide a good framework for high throughput
and simultaneous screening of high density catalytic libraries.

45

When the high temperature microelectrode REMPI spectra of the product
molecules do not have distinguishing features or have features exhibiting overlap,
products must be cooled to improve REMPI spectra. This can be readily accomplished,
30 as shown in Fig. 7, by expanding a portion of the product gas plumes 41 emanating from
the library sites 33 into vacuum chamber 42 through small orifices 43. Portions of the
50 product gas directed through orifices 43 undergo adiabatic expansions forming

55

5 supersonic jets in vacuum chamber 42 thereby decreasing the gas temperature resulting
in significant simplification of the REMPI spectra. In addition, as shown in Fig. 7,
10 precooling thermal exchanger may be located upstream of orifices 43 to reduce the
temperature of the product gases prior to passage through orifices 43. Gas flow into a
15 vacuum chamber can also be pulsed to improve the pumping requirements. For an ideal
gas with a heat capacity ratio γ , that is $\gamma = c_p/c_v$, the temperature of the gas is related to
pressure by the following relationship under adiabatic conditions: $T_2 = T_1(P_1/P_2)^{(1-\gamma)}$
wherein T_1 , P_1 and T_2 , P_2 are the initial and final temperatures and pressures, respectively.
For example, for $\gamma = 1.4$ and an initial temperature of 800 K and 760 Torr pressure, the
20 temperature of the adiabatically cooled gas expanded into a vacuum at 10^{-3} Torr will be:

$$T_2 = 800 (10^{-3}/760)^{(1.4-1)/1.4} = 16.7 \text{ K}$$

25 This temperature is suitable for generation of an excellent REMPI spectra.
15 Castaldi, M.J. and Senkan, S.M., 1998, *supra*. Simultaneous product screening of the
catalyst library can be achieved by photoionizing the products using laser beam(s) 23,
30 followed by detection of photoelectrons or photoions using microelectrodes 27 placed
inside vacuum chamber 42 in close proximity to the expanding jet.

35 Fig. 8 schematically shows a flat plate solid state catalyst library containing
seventy two test sites 21, arranged 8 rows wide by 9 rows axially which are sufficiently
separated from one another to result in minimal intersite diffusion of product gases,
within reactor 45. Contact of reactants with the catalytic test sites is achieved by use of
40 reactant feed tubes 34, as described with reference to Fig. 3, which effectively mask the
upstream catalyst sites. Each of the test sites in a row being screened has a dedicated
25 microelectrode 27 for product gas detection, eight as shown in Fig. 8, for screening by
row. Arranging the test sites in rows expedites screening in a row-by-row fashion using
a single laser beam and provides simultaneous screening of eight sites. Any row size can
45 be accommodated using this invention. However, any library pattern having specific
addresses for individual test sites can be screened by moving the library with a computer
50 controlled two-dimensional translation device. The smallest site size, providing the
highest library density, is determined by the gas phase dispersion rate of product gas
between test sites. Consequently, different products can allow the generation and testing

5 of different library densities. In the row screening process, as exemplified in Fig. 8, laser
beams 23 pass through window 39 of reactor 45 and through the product gases above
the test sites 21, perpendicular to the reactant gas flow from reactant feed tubes 34 and
passes through the product gas plumes of all of the sites in a row, as indicated by the
10 dotted line, and exits reactor 45 to laser beam dump 46. Reactant feed tubes 34 are
supplied by reactor gas supply manifold 48. In Fig. 8, two lasers are indicated, however,
any number of lasers may be used in a given application. Based upon the numerical
15 design example given above, positioning of the laser beam about 5 mm above the
substrate surface should be adequate for the laser beam to intercept the product plume
20 and generate photoions, if a product is formed. Product gas exits reactor 45 through gas
outlet 49. However, the laser beam may be placed anywhere in the product plume to
maximize signal generation. It is apparent that if the test site is not catalytic, no product
formation and therefore no photoionization will take place. Photoions and
25 photoelectrons generated are collected by the microelectrodes 27 positioned in close
position above the laser beam. Based upon the above numerical design example,
30 microelectrodes can be positioned anywhere beyond 5 mm above the test site surface and
close to the laser beam to maximize signal intensity. However, microelectrodes can be
placed at different positions above the test sites to maximize signal collection in
conjunction with the local fluid dynamics of the product plume. As noted above, the
35 library substrate can also serve as the ground or cathode, or a microelectrode can be
placed through a nonconductive substrate, if necessary, or microelectrodes can include
both the anode and cathode as shown in Fig. 8. The microelectrodes are powered from
DC power source 30 through a multichannel switch and the measured signal of each
40 microelectrode fed to detector 31. After testing of a particular row, the library can be
25 moved either upstream or downstream, using library translator 47, to position the next
row of sites for catalytic screening.

45 Another embodiment of this invention to exemplify the row screening process is
shown in Fig. 9. The embodiment shown in Fig. 9 is similar to Fig. 8 except that porous
catalyst libraries having porous test sites 21p are fed reactant gas from a plenum beneath
30 them which is supplied reactant gas through reactant gas supply inlet 50. The reactant
gas passes through porous test sites 21p forming a plume above each test site
50 simultaneously as indicated by the arrows. The reactor can be rotated 180° around the

5 x-axis, if desired, to enhance product detection by altering the natural convective processes in the reactor vessel. As shown in Fig. 9, screening is done on a row-by-row 10 in similar manner as described with respect to Fig. 8. Alternatively, screening of all sites simultaneously may be done by equipping each site with a dedicated microelectrode and 15 providing the ionizing laser beam 23 to pass all sites simultaneously using turning mirrors 26, as shown in the top view of Fig. 10. Optical fibers may also be used to direct the laser beam to all sites simultaneously. Signals from the microelectrodes are then 20 detected and recorded by a dedicated detector for each site on catalyst library 51 or by use of a computerized multichannel switching system 65 to rapidly and sequentially 25 detect the signal coming from each site. It is apparent that any catalyst library size and shape can be accommodated and operated in this simultaneous screening mode as long as 30 each site is individually addressable.

Another embodiment of this invention is shown in Fig. 11 which schematically 25 shows a 16 by 16 or 256 site monolith structure 40 as described with respect to Fig. 7 30 15 forming a solid state catalyst library. Any monolith cell density can be used. Reactant gases are provided through reactant gas supply inlet 50 to a manifold beneath the library and pass upwardly through the channels, passing over or through catalysts, generating 35 product plumes which may be measured within the channels as shown in Fig. 6, above the exit from the channels as shown in Fig. 9, or following cooling by a supersonic jet 20 into a vacuum chamber as shown in Fig. 7. Catalyst screening may be accomplished 30 using row-by-row method as shown in Fig. 11 or by screening all sites simultaneously as 35 described with respect to Fig. 10.

Another embodiment of a monolith supported catalyst library screening structure 40 within a reactor is shown in Fig. 12, generally using the arrangement as described with 25 respect to Fig. 6. As shown in Fig. 12, a separate catalyst library monolith 55 having 72 45 sites and a separate catalyst screening monolith 56 forms the catalyst screening structure within reactor 45. A dedicated microelectrode 27 is provided inside of each monolith channel. Upstream of each microelectrode 27, optical access to each channel is provided 50 by laser access windows 39. Reactant gases are introduced by reactant gas flow 30 distributor and enter each of the individual library channels, as indicated by the arrows, to pass over the catalyst sites. Products are detected downstream inside the screening monolith 56. Lasers emanating from tuneable laser sources 24 and/or 25 are directed to

5 each row of the screening monolith 56 via beam splitters 52 and through laser windows 39 to pass through each of the channels in the row through the internal laser windows as shown. This arrangement provides simultaneous screening of all sites in the library.

10 Different laser beams can be directed to different rows in the screening monolith 56 to 15 screen for different products. This technique can also be applied for screening other library configurations. Fiber optic lines 53 can also be used to direct the laser beam to the library sites. If product cooling is desirable, this can be accomplished by adiabatically 20 expanding the product gas plumes into a vacuum chamber through small orifices, as shown in Fig. 7.

25 In the above description of catalyst screening apparatus and techniques the temperature has been the same at all catalyst sites, which would be appropriate for screening for new catalysts or to modify catalysts. It is possible, according to this invention, to construct catalyst libraries having individually temperature controlled sites 30 wherein different sites would be maintained at different temperatures or their 35 temperatures could be programmed to follow a specified temperature-time program. Such differing temperatures generates information on the effects of reaction temperatures on catalyst activity and selectivity. Using micromachining, individually temperature controlled and programmable sites may be economically constructed, such as done for 40 thermal inkjet printer heads. It is readily apparent that the amount of insulation provided by the substrate and the temperature programming demands influence the intersite 45 spacing and the density of the catalyst libraries with temperature controlled sites.

50 It is also possible to screen an entire catalyst library using a batch mode operation. In the batch mode, the entire catalyst library is first isolated from the reactant gases by a physical mask. The test chamber is then purged and filled with fresh reactant 55 gases. The chamber contents are allowed to reach thermal equilibrium which can be monitored by thermocouples placed within the test chamber. The physical mask is then removed exposing either a specified section or the entire catalyst library to reactant 60 gases. Since there is no forced convection, diffusion and natural convection are the major modes of gas transport in the test chamber. The sites that are catalytic then 65 generate reaction products which diffuse into the bulk gas phase generating a product concentration plume. For a constant concentration of the product, the concentration 70 penetration depth, $\delta_c(t)$, can be approximated by the relation:

$\delta_c(t) = (12Dt)^{1/2}$ where D is the diffusivity and t is the time. The concentration penetration depth must be kept less than the intersite spacing to prevent overlapping of concentration plumes from adjacent sites resulting in signal crossover. For a flat plate catalyst library, assuming 1 cm intersite spacing, $\delta_c = 1$ and $0.1 \text{ cm}^2/\text{sec}$ for gas

5 diffusivity, the REMPI measurements for the entire library must be completed in about 1 second to avoid overlap of concentration boundary layers. Available fast electronic

equipment can meet these requirements. Larger site dimensions and/or placing physical barriers between sites can significantly decrease intersite diffusion-mixing rates, thereby providing longer times for measurements. In the case of monolith structures, physical

10 walls existing between the sites substantially decrease intersite diffusion, thereby allowing acquisition of data for longer periods of time by microelectrodes placed near or inside the channels for detection of photoions and/ or photoelectrons created by the laser beam.

An advantage of the batch system is that it can be used to simultaneously screen all sites in the solid state catalyst library.

One embodiment of a homogeneous catalyst library which can be synthesized, as described earlier, and screened according to this invention is shown in Fig. 13 wherein

catalyst solution 57 is maintained in container 58 and reactant gases are bubbled through the liquid. Gas dispersion through the liquid catalyst can be achieved in any suitable fashion as will be apparent to one skilled in the art, for example, pressurised reactant gases can be fed through reactant plenum 36 and forced through a controlled porosity distribution plate at the bottom of the sample site, as shown on the left in Fig. 13.

Alternatively, reactant gases from reactant plenum 36 may be bubbled through a capillary sparger 60 at each sample site, as shown on the right in Fig. 13. Gaseous products 22 formed leave the liquid catalyst solution, as indicated by the arrows in Fig. 13, and

product gas detection performed in any of the manners described earlier. The minimum diameter of container 58, which controls the library density, must be established from considerations of the surface tension and viscosity of catalyst solution 57 which influence the extent of gas dispersion and liquid carryover.

Fig. 14 is a schematic showing of catalyst library screening using a homogeneous liquid catalyst library, as described with respect to Fig. 13, within reactor 45. REMPI catalyst screening can be either on a row by row basis, as illustrated in Fig. 14, or the entire catalyst library can be screened simultaneously, using the method as described with

5 respect to Fig. 10. The reactor system exemplified in Fig. 14 may also be used to screen
10 solid catalyst powders which can be placed in the container, as will be described in
15 further detail with respect to Fig. 15.

10 Solid particles may be incorporated into the liquid catalyst library to achieve three
5 phase, gas-liquid-solid, operating conditions. The introduction of solid particles 60 to
15 the liquid in container 58 enhances gas dispersion, forms smaller gas bubbles 61 to
20 provide better gas-liquid contact and improves reactant conversion, thereby increasing
25 the speed of library screening, is shown in the left hand portion of Fig. 15. The bed can
30 also be fluidized, partially or fully, under the screening conditions. Product gases 22,
35 indicated by arrows, emanate from container 58 and may be analyzed by any of the
40 REMPI methods previously described. The solid particles used may be catalytic, thereby
45 providing the opportunity of screening multi-phase catalytic reactions. Homogeneous
50 liquid catalysts may also be placed into porous particles, for example to immobilize
55 proteins or molten salt catalysts, in the systems as shown in Fig. 15. Solid catalytic
60 particles 62 may be introduced into container 58, without liquid, to achieve gas-solid
65 operating conditions, as shown in the right hand portion of Fig. 15. Catalyst powders,
70 prepared in a number of different manners, can be placed within the container shown in
75 Fig. 15 to create a micro packed bed reactor library. Reactant gases may be introduced
80 to the packed bed reactors through plenum 36 and products formed detected using the
85 REMPI microelectrode systems previously described.

90 Fig. 16 is a schematic showing of another catalyst screening method using
95 catalyst particles in a monolithic library. Catalyst particles or powders 62, prepared in a
100 number of different ways, can be placed into the cells of monolithic structure 40. The
105 reactant gases are then passed through the packed bed of catalyst particles 62 and are
110 discharged through a small channel/orifice 43 into vacuum chamber 42. The product jets
115 then undergo expansion cooling and are subjected to laser beam 23 for the generation of
120 photoions and photoelectrons. The photoions or photoelectrons generated are then
125 detected by microelectrodes 27, as described above.

130 The magnitude of the REMPI signals produced by the photoionization of product
135 species will be proportional to their concentration. In addition, the generated signals are
140 also influenced by the operational parameters, such as, the power of the UV laser used,
145 the DC bias voltage applied to collect the photoions/photoelectrons, the separation

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5 distance of the anode and cathode and the position of the microelectrode relative to the
laser beam. Once optimized for the particular system to be used for catalyst library
screening, the operational variables can be fixed so that the measured REMPI signals can
be directly attributed to produce concentrations generated by the catalyst sites.
10
15 5 Consequently, in addition to the qualitative, active versus inactive, screening of catalyst
libraries, the REMPI microelectrode technique of this invention can be used to
quantitatively rank the activities and selectivities of catalysts. Catalytically more active
sites will produce higher concentration of products in the product plume and thereby
generate larger REMPI signals, and likewise, less active catalyst sites will generate lower
10 concentrations of products and thereby lower REMPI signals. In catalyst library
20 quantitative screening, gas mixtures containing known concentrations of product gases
are first passed sequentially over the library under conditions at which no reactions take
place and the microelectrode responses noted. Using microelectrode responses to
known product concentrations, calibration of each site and microelectrode may be
25 achieved. These calibration functions are then used to determine the quantitative
concentrations of products formed during the active catalyst screening process. If the
catalyst loading is different at different library sites, this also must be accounted for in
30 ranking of the catalytic activity of the sites. Alternatively, internal standards can be
added to the reactant feed stream during the screening process to expedite the
20 quantification of the activities and selectivities of catalyst sites.

35 The catalyst screening techniques disclosed can be utilized to obtain a greater
spectrum of objectives. Two or more laser beam energies can be used sequentially to
monitor two or more reaction products in a product plume, which is important to
establish catalyst selectivity and to discover multifunctional catalysts. For example, the
40 25 development of catalysts which not only maximizes the formation of specific products
but also minimizes the formation of by-products or pollutants is an increasingly important
objective in environmentally conscious manufacturing. In the practice of this invention, a
series of laser pulses, each pulse specifically photoionizing a selected molecule, can be
45 30 used to sequentially monitor different products. Since laser photoionization and product
detection are fast processes, having time scales in microseconds, rapid screening of large
potential catalyst libraries for multifunctional catalytic activity can be accomplished even
50 with the sequential detection of a large number of species.

5 In some applications, the products formed by the catalytic reaction may be in the
10 liquid or solid state, for example, reactions of high molecular biomolecules catalysed by
 enzymes, thus the direct application of REMPI is not suitable to screen catalytic activity
 and selectivity. The REMPI method, however, can be applied if the reaction products
15 are first gasified. This can be accomplished by using a pulsed ablation laser, such as a
 pulsed CO₂ or excimer laser, to rapidly gasify product molecules from a liquid or solid
 surface. One embodiment using an ablation laser is shown in Fig. 17 wherein ablation
20 laser source 63 generates ablation laser beam 64 to rapidly gasify product molecules
 from the surface of liquid catalyst solution 57 into gaseous product plume 22 which may
 be intercepted by ionization laser beam 23 and produced photoions and photoelectrons
 detected by any of the microelectrode methods described above.

25 It is evident from the above disclosure, that it is also possible to monitor reaction
 intermediates as well as reaction products using the REMPI microelectrode methods of
 this invention. The ability to monitor reaction intermediates, as well as products, greatly
30 enhances the range of applicability of the methods of this invention. In addition, because
 measurements according to this invention can be undertaken in real time without any
 delay, fast transient processes can be monitored. This capability then leads to better
 understanding of the catalyst function and thus aids in the development of new and
 improved catalysts.

35 20 The following specific example is set forth in detail to specifically demonstrate
 this invention and should not be taken to limit the invention in any way.

40 35 The catalyst screening method of this invention was used in the catalytic
 dehydrogenation of cyclohexane into benzene according to the reaction C₆H₁₂ → C₆H₆ +
 3H₂. This is a well established reaction which is catalyzed by transition and precious
45 25 metals in the temperature range of 250° to 350°C. Rebhan, D.M. and Haensel, V., "A
 Kinetic and Mechanistic Study of Cyclohexane Disproportionation: An Example of
 Irreversible Hydrogen Transfer", J. Catalysis, 111, 397, 1988.

50 45 Supported Pt and Pd catalysts, 0.5% and 1.0% Pt and Pd on activated carbon,
 were obtained from Precious Metals Corp. These catalysts, as well as several inert
 30 carrier materials, silica and alumina, were then incorporated into one row in a library
 substrate in 5 mm by 5 mm cells similar to Fig. 5. The addresses for the catalysts and
 inert carrier materials were:

5

Site No.	1	2	3	4	5	6	7	8
Material	Inert	0.5%Pt	Inert	1.0%Pd	Inert	Inert	1.0%Pt	0.5%Pd

10

The catalyst library was then placed into a reactor and heated to 300°C in the presence of an argon gas flow. Following establishment of the steady state operating temperature, which was determined by thermocouples inside the reactor, a cyclohexane reactant stream was introduced. The reactant stream composition was 13% cyclohexane in argon gas which was prepared by bubbling argon gas through cyclohexane liquid at about 25°C by using a sparger.

20

The library screening process demands the unambiguous detection of benzene in a cyclohexane, hydrogen and argon mix. A suitable UV laser wave length for selectively producing benzene REMPI ions was identified in separate tests using a laser photoionization time of flight mass spectrometer, TOF-MS. Gas pulses of cyclohexane and benzene, each at a concentration of about 500ppm in argon, were expanded into the vacuum chamber of the TOF-MS using a pulsed valve and the resulting jet/molecular beam was crossed by a pulsed UV laser beam in the 258-262 nm range to generate their photoionization and mass spectra. The UV laser had about 100μJ/pulse energy and was obtained from the dye laser using Coumarin 500 dye. These measurements led to the conclusion that the REMPI ions produced by the 258-262 nm UV laser were exclusively due to photoionization of benzene, mass 78, with no photoions detected at masses 84 for cyclohexane or 40 for argon or 2 for hydrogen. No peaks other than the benzene parent at mass 78 were detected. Fig. 18 shows the REMPI spectrum of benzene and cyclohexane as determined by the TOF-MS technique. It is evident from Fig. 18 that benzene exhibits a major REMPI peak starting at 259.7 nm, where there is no contribution from cyclohexane.

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REMPI spectra of benzene and cyclohexane were also determined at 1 atm and ambient temperature using the microelectrode process. Cyclohexane and benzene in argon carrier gas were photoionized by passage of a pulsed UV laser beam in the 258-262 nm range within 1-2 mm of the probe tip. A DC bias of +500 V from a power source was applied to the anode to collect the photoelectrons. The resulting REMPI spectra are shown in Fig. 19 and are similar to the spectra obtained by the TOF-MS

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5 shown in Fig. 18, with expected spectral broadening observed in the ambient temperature
and 1 atm. pressure conditions. This shows that use of the 259.7 laser results in the
10 exclusive and efficient production of benzene REMPI ions in the presence of
cyclohexane, argon and hydrogen in the reactor system.

15 5 The reactor system shown in Fig. 9 was used passing cyclohexane in argon
carrier gas through the eight library sites in a row, as identified above. The 259.7 nm
laser beam was passed through the product plume from the library sites and the benzene
REMPI signals detected in the vicinity of each of the eight sites are shown in Fig. 20.
These measurements correspond to data acquired by one laser shot and the signals
20 10 exhibited fast rise and decay time, in the order of microseconds. As evident from Fig.
20, microelectrodes located at sites 2, 4, 7 and 8 picked up appreciable benzene signals,
consistent with the presence of Pt and Pd catalysts at these sites. While some REMPI
signals were also detected at sites 1, 3, 5 and 6, they were significantly lower, consistent
25 15 with the absence of catalysts at these sites. Evidently some benzene was present in the
reactor bulk gas due to low gas flow rates and recirculation patterns present in the
reactor, both of which reduce the rapid removal of reaction products from the reactor. A
smaller reactor chamber, use of monolithic structures or other library designs would
30 20 reduce this problem. Nevertheless, Fig. 19 shows that the method of this invention
rapidly and clearly distinguished between active and inactive sites in the library. The
reactor exhaust gases were also analyzed by the TOF-MS using the 259.7 nm laser beam
35 25 during screening to ascertain whether species other than benzene could have contributed
to the measured microelectrode signals. No photoions other than those with mass 78
were detected.

40 30 Based upon the magnitude of the REMPI signals measured, as shown in Fig. 20,
25 45 the relative activities of the catalytic sites appear to be $7 > 2 > 4 > 8$. These results are
consistent with the relative loadings of the Pd and Pt commercial catalysts at these sites,
and also suggest that Pt is a more active cyclohexane dehydrogenation catalyst than Pd.
These findings are in agreement with results using conventional catalytic reactor systems.
45 Rehbon, D.M. and Haensel, V., 1988, *supra* and Ahmed, K. and Chowdhury, H.M.,
30 "Dehydration of Cyclohexane and Cyclohexene over Supported Nickel and Platinum
Catalysts", *Chem. Eng. J.*, 50, 165, 1992.

50 55 It should be recognized that the conditions specified in the above description and

5 example are meant to illustrate the application of the catalyst screening technique of this
invention. One skilled in the art can infer from this description and example that the
method of this invention can be used to screen any catalyst for any reaction. The
10 reaction conditions can be broadly varied without change in the screening method. For
5 example, the reaction temperature can easily be varied from room temperature, such as
25°C., to higher temperatures, such as 1000°C. Similarly, the pressure can be varied
from vacuum, such as 10^4 Torr, to high pressures, such as 500 atmospheres. The
15 screening process can easily accomodate a wide range of reactant feed concentrations
from pure components, 100%, to very dilute streams, such as a few hundred parts per
10 million, 100 ppm.

20 Combinatorial catalyst libraries can also be generated by machining miniature
reactors using integrated circuit manufacturing steps such as thin film deposition,
lithography, etching, plasma processing and the like. This approach has been used
recently to make a reactor on a chip for the catalytic oxidation of ammonia, as described
25 in Srinivasan, R., Hsing, I.M., Berger, P.E., Jensen, K.F., Firebaugh, S.L., Schmidt,
M.A., Harold, M.P., Lerou, J.J. and Ryley, J.F., "Micromachined Reactor for Catalytic
Partial Oxidation Reactions", AIChE Journal, 43, 3059-3069, 1997. Unlike monolithic
30 or honeycomb structures which are passive, the micromachined reactors can also
incorporate flow and temperature sensors, heating elements and actuators for the control
20 of operating conditions. In this invention, a large number of microreactors are prepared
in parallel using any suitable integrated circuit manufacturing sequence. Each
35 microreactor system includes passages for reactant feed, catalytic reaction, product exit,
and radiation access. These passages can be machined by either wet or dry etching of an
inert wafer substrate, such as silica or alumina, or materials which are coated by such
40 inert films, for example, metals coated by inert materials. The exit passage of each
reaction zone should be large enough to accommodate a microelectrode for detection of
product REMPI ions. Sensing, flow and temperature controllers can also be embedded
45 into the individual reactor sites on the wafer. In addition, electrical circuitry can be
- embedded to electrochemically control the catalytic reactions. Different catalytic
30 materials can be deposited into different reactor passages of the library by a variety of
techniques, such as, for example, sputtering, laser ablation, thermal or plasma enhanced
50 chemical vapor deposition, and the like, with the use of masks. Alternatively, catalysts

5 can be deposited into the reactor passages using solution techniques with the aid of
micro-jet or micro-drop dispensers. These dispensers can also be used to deposit slurries
containing catalyst particles. When using solution techniques, the reactor passages can
be modified in the reaction zone to contain the necessary amounts of liquid and/or slurry
10 catalyst precursors. This can be accomplished, for example, by machining a reservoir in
a central region of the reactor passage for collection of liquid or slurry catalyst precursor
mixtures. These reservoirs may be of any shape and can also have internal baffles,
15 actuators and sensors to better control the preparation of catalysts and operation of the
reactors during the screening process. The reservoirs can also be placed at different
10 locations along the microreactors to control pressure drop, reactant preheat and product
20 quench conditions. Liquid and/or slurry mixtures of catalyst precursors may be
introduced into the reservoirs using micro-jet or micro-drop dispensers and robotics.
Following the addition of the liquids, agitation may be induced, for example, by
25 mechanical vibration, micro-activators or sonication, to assure mixing of the liquid or
15 slurry mixtures. After dispensing the catalyst precursors, the resulting mixtures are
thermally and chemically treated for the formation of catalysts. These treatment
processes may include drying, calcining, oxidation, reduction and activation.

30 Figs. 21 and 22 are simplified schematic showings of bases for single
microreactor systems according to this invention. Fig. 21 shows a microreactor suitable
20 for thin film or solid particle catalyst deposition processes and Fig. 22 shows a
microreactor additionally suitable for solution based catalyst deposition processes. In the
35 figures, inert microreactor body 70 has reactant feed passage 71 leading to a catalyst
zone, shown in Fig. 21 as zone 72 and in Fig. 22 as enlarged reservoir catalyst zone 73.
As shown in Fig. 22, baffle structure 74 may be located in reservoir 73. Such baffle
40 structures may have a number of effects, such as, providing additional exposed surface
area for the catalyst and for inducing mixing to benefit some reactions. Products exit the
reaction volume through exit passage 75. Reactant feed and product flow are shown by
45 the arrows. Activating radiation passages 76, having optical access windows for
isolation of exit passage 75, are provided to direct passage of activating radiation beam
50 77 through the product stream passing through exit passage 75. Fig. 21 shows external
microelectrode 78 and Fig. 22 shows internal microelectrode positioned in exit passage
75 in proximity to the activating radiation beam 77 to collect photoelectrons or

5 photoions for detection, as previously described. Internal microelectrode 84 is attached
to microreactor body 70, such as embedded to the bottom, side or top walls of the
10 product exit passage, and is thus an integral part of the microreactor body. These
internal microelectrodes may be flush with the product exit passage walls or may
15 protrude from them. The internal microelectrodes are provided with suitable wiring for
powering the microelectrodes and for passage of detected signals to a detection
measurement device. These wirings and connections are embedded in the microreactor
body during fabrication using established microelectronics manufacturing techniques.

Fig. 23, wherein the numerals referred to above have the same meaning,
10 schematically shows an array of microreactors in a single inert microreactor body 70.
Any number of microreactors may be present in the array, depending upon the size of the
20 microreactors and the physical characteristics of the substrate wafer. Each microreactor
72 can be of any size, however, reactor channels in the order of about 0.1 to 2
25 millimeters wide are most suitable for fabrication and subsequent screening processes.
Reactant plenum 79 is in fluid communication with each reactant feed passageway 72 to
30 distribute reactants to each microreactor. Reactant plenum 79 is sufficiently large to
insure the establishment of similar fluid flow rates through each microreactor, provided
35 that the pressure drop characteristics of the microreactors are similar. Alternatively, flow
sensors and actuators may be fabricated in each microreactor to independently control
40 fluid flow through each of the microreactors. A different catalyst may be placed in each
microreactor using, for example, any of the techniques described. The physical forms of
45 these catalysts can be films, as indicated by numeral 86, or powders, as indicated by
numeral 85. Fabrication of a microreactor array from a single base wafer insures good
50 alignment of the activating radiation passages 76 and microelectrodes 84, thereby
expediting the screening process. Internal electrodes 84 make possible internal wiring for
powering the microelectrodes and for passage of detection signals to a detection
measurement device. Alternatively, separate and different electrodes, one for the anode
45 and one for the cathode, can be embedded to different walls of the reactor for powering
and signal detection. Suitable connectors may be located on the exterior of the array for
30 easy connection of the entire array to a power source and a detection measurement
device through selective switching. Reactant feed and product flows are shown by the
arrows.

5 Following fabrication of the microreactor base layer, an inert cover wafer 80 is
bonded to inert microreactor base 70 to cover the microreactor array, as shown in Fig.
10 24, to isolate each microreactor system while allowing the flow of reactant in and the
flow of products out of the microreactor array. Fig. 24 shows internal microelectrodes
15 87 attached to or embedded in cover wafer 80 in similar manner as described with
respect to internal microelectrodes 84 attached to microreactor body 70, as disclosed
above. Internal wiring 88 leads from each microelectrode 87 to external connector 89 for
powering each microelectrode and for passage of detection signals from each
microelectrode to a detection device. Alternatively, separate electrodes can be
20 embedded to the base 70 for signal detection and/or for power supply. Heating elements
may be embedded in thermal conducting microreactor body 70 between microreactor
chambers 72 and/or in thermal conducting cover wafer 80 and/or in thermal conducting
sheets between stacked reactor arrays to provide desired temperature control to the
25 microreactors and/or reactant feed channels. As shown in Fig. 25, individual flat
15 microreactor arrays, as shown in Fig. 24, may be stacked vertically to obtain three
dimensional structures of a plurality of flat microreactor arrays, thereby providing rapid
30 analysis of a large number of samples in the manner similar to that shown in Fig. 12. The
microreactor arrays may have any suitable fasteners for maintaining adjacent arrays in
fixed relationship with each other. The microelectrodes are powered by DC power
20 source and the signal from each microelectrode fed through a multi-channel selector to
measurement device.

35 Fig. 26 shows a microreactor array 91, as shown in Fig. 24, may be placed in
microreactor array frame 92 for easy handling and connection for catalyst screening.
The microreactor array fits into an opening in the frame as indicated by the reversible
40 25 arrow. Reactant feed is provided through the frame to the reactant feed manifold of the
microreactor array, as indicated by the arrows, and product exits through the frame, as
indicated by the arrows. Radiation passages 93 are provided through frame 92 for entry
45 and exit of radiation beam 77 aligned to pass through radiation passages 76 in
- microreactor body 70, as described above. The frame also has internal wiring 94 for
30 connection at one end to internal wiring 88 of the microreactor array and at the opposite
end to a power source and a detection measurement device. The internal wiring of a
50 plurality of microreactor array frames may connect through a single connector to

5 external wiring. The frames may also have reactant feed manifolds arranged so that a single feed supply can provide reactant to a plurality of microreactor array - frame assemblies. The frames may also provide temperature control for the microreactor array through heating elements built into the frames. Microreactor array - frames may have
10 5 any suitable means for connection of adjacent microreactor array frame assemblies.

A plurality of microreactor - frame assemblies may be joined in a vertical fashion similar to that shown in Fig. 25. In another embodiment, shown in Fig. 27, microreactor array - frame assemblies 95 may be joined horizontally in side-by-side relation.

15 Alignment of radiation passages 93 makes it possible to use one radiation beam 77 in the 10 evaluation of large catalyst libraries.

20 Screening is accomplished by passing a known amount of reactant gases through the microreactor array in contact with the potential catalysts forming reaction products which are activated by passing a suitable tunable radiation beam through activating
25 radiation passages 76, having access windows providing fluid isolation, to form product

15 REMPI ions in the product exit passages 75. These product REMPI ions are detected by the microelectrodes within the exit passages and measured in manners described above. During screening, the microreactor arrays may be placed in a furnace for
30 temperature control of the entire array or the temperature of each microreactor may be independently controlled using sensors and heating elements built into the microreactors
20 during the microreactor fabrication process. Alternatively, temperature control can be provided by the frame.

35 Figures 28A and 28B summarize another example of combinatorial catalyst library preparation and screening method using a different microreactor array and
40 microdrop/microjet technology according to this invention. Step 1 shows preparation of
25 the catalyst library inert substrate using a plug to form desired passageways and to retain liquid during solution deposition. Step 2 shows catalyst precursor solution deposition into reservoirs of catalyst reaction zones. Step 3 shows drying and calcining of the
45 catalyst by methods well known in the art. Step 4 shows opening of the product exit
30 passageways by removal of the plugs used to form the passageways. Step 5 shows formation and/or activation of the catalyst by passage of a suitable gas through the microreactor array. Step 6 shows screening of the catalysts within the array of microreactors by
50 passing reactant gas(s) in contact with the catalyst in each microreactor, passing a

5 radiation beam of an energy level to promote formation of specified ions through each reaction product stream, and detecting the formed ions or electrons by microelectrode collection in proximity to the activating radiation beam.

10 While in the foregoing specification this invention has been described in relation

15 to certain preferred embodiments thereof, and many details have been set forth for purpose of illustration it will be apparent to those skilled in the art that the invention is susceptible to additional embodiments and that certain of the details described herein can be varied considerably without departing from the basic principles of the invention.

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Claims

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I Claim:

20 1. A microreactor and sampling probe system for mass spectrometric screening of catalytic and potential catalytic reaction products, said system comprising; a plurality of addressable microreactors, each comprising, an inert substrate body, a reactor passageway extending from a first opening on one side of said substrate body to a second opening on the opposite side of said substrate body, a reaction zone in the central portion of said reactor passageway serving as a reaction zone for contact of reactants with a catalyst in said reaction zone, a reactant zone of said reactor passageway extending from said reaction zone serving as a reactant feed passage, and a product zone of said reactor passageway extending from said reaction zone to said second opening serving as a product exit passage; a tubular sampling probe comprising at one end a sampling orifice forming a free jet expansion stream into a substantially expanded chamber of at least one vacuum stage and an open opposite end connectable to an inlet orifice of a mass spectrometer; and a translation mechanism capable of placing said sampling orifice in proximity to said product exit passage of an addressable single microreactor for a sampling mode and rapidly translating to position said sampling orifice in a position in proximity to the product exit passage of a second addressable single microreactor for a sampling mode of said second microreactor.

25 10 2. A system according to Claim 1 wherein said sampling orifice is about 1 to about 200 micrometers in diameter located at the vertex of an expansion cone having a half cone angle of about 15 to about 45 degrees.

30 15 3. A system according to Claim 1 wherein said sampling orifice is a short capillary having a diameter of about 1 to about 500 micrometers and a length of about 1 to about

35 40 45 50

5 200 micrometers.

10 4. A system according to Claim 3 wherein said capillary has a diameter of about 5 to about 20 micrometers and a length of about 50 to 100 micrometers.

15 5. A system according to any one of the preceding Claims wherein the distance from said sampling orifice to said inlet orifice of said mass spectrometer is about 3 to about 10 inches.

20 6. A system according to any one of the preceding Claims wherein said expanded chamber comprises two vacuum stages having a skimming orifice between a first and second vacuum stage.

25 7. A system according to any one of the preceding Claims wherein said microreactor additionally comprises a radiation beam passageway extending through said substrate body generally perpendicular to and intersecting said product zone, said radiation beam passageway having radiation beam access windows providing passage of a radiation beam and fluid isolation of said radiation passageway from said product zone; and a microelectrode in said product zone in proximity to the intersection of said radiation beam passageway with said product zone.

30 8. A system according to any one of the preceding Claims wherein said plurality of microreactors is an in-line array of microreactors fixidly mounted on a translation table rapidly movable along an x axis for alignment of said sampling orifice and said product exit passage and along a z axis for placement of said sampling orifice and said product exit passage in proximity to each other.

35 9. A system according to any one of the preceding Claims wherein said plurality of microreactors is a parallel stack of a plurality of in-line arrays of microreactors fixidly mounted on a translation table rapidly movable along x and y axes for alignment of said sampling orifice and said product exit passage and along a z axis for placement of said sampling orifice and said product exit passage in proximity to each other.

40 25 10. A system according to any one of the preceding Claims wherein each said microreactor comprises temperature and flow controls for individual control of temperature and flow in each microreactor.

45 30 11. A system according to any one of the preceding Claims wherein each said microreactor comprises an insert for placement in and removal from said reaction zone for catalyst loading.

5 12. A process for rapid screening of potential catalyst libraries for catalytic properties, comprising: forming a potential catalyst library having potential catalysts at a plurality of addressable test sites; passing reactant gas in contact with said potential catalysts in at least one of said plurality of addressable sites; and screening gas plumes of

10 5 reaction products from said addressable sites, said screening comprising translating at least one of a sampling probe and said library to a position that one addressable site is in proximity to a sampling probe orifice, passing a portion of said reaction products from said one addressable site through said sampling probe orifice forming a free jet expansion stream in a substantially expanded volume of at least one vacuum stage thereby cooling

15 10 and reducing the pressure of the jet stream of said reaction products to a pressure suitable for introduction into a mass spectrometer, and passing a portion of the jet stream of reaction products at reduced pressure through an inlet orifice into a mass spectrometer for analysis.

20 13. A process according to Claim 12 wherein said sampling probe orifice is about 1 25 15 to about 200 micrometers in diameter located at the vertex of an expansion cone having a half cone angle of about 15 to about 45 degrees.

30 14. A process according to Claim 12 wherein said sampling probe orifice is a short 35 20 capillary having a diameter of about 1 to about 500 micrometers and a length of about 1 to about 200 micrometers.

40 20 15. A process according to Claim 14 wherein said capillary has a diameter of about 5 to about 20 micrometers and a length of about 50 to 100 micrometers.

45 16. A process according to any one of Claims 12 to 15 wherein the distance from said sampling probe orifice to said inlet orifice of said mass spectrometer is about 7.5 to about 25 centimeters.

50 25 17. A process according to any one of Claims 12 to 16 wherein said expanded chamber comprises two vacuum stages having a skimming orifice between a first and second vacuum stage.

18. A process according to any one of Claims 12 to 17 additionally comprising 45 30 passing at least one radiation beam of an energy level to promote formation of energized products comprising specified ions and electrons through said gas plume of reaction products and detecting in real time said formed ions or electrons by microelectrode collection in situ in proximity to said addressable sites.

5 19. A process according to Claim 18 further comprising contacting said products f
reaction with at least one energy beam forming fragmentation daughter product(s) and
said screening and said detecting is performed on said fragmentation daughter
product(s).

10 5 20. A process according to any of Claims 12 to 19 wherein said plurality of
addressable test sites comprise microreactors in a parallel stack of a plurality of in-line
arrays of microreactors fixidly mounted on a translation table rapidly movable along x
15 and y axes for alignment of said sampling probe orifice and a reaction product exit
passage from a single addressable microreactor and along a z axis for placement of said
10 10 sampling orifice and said product exit passage in proximity to each other.

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FIG. 1

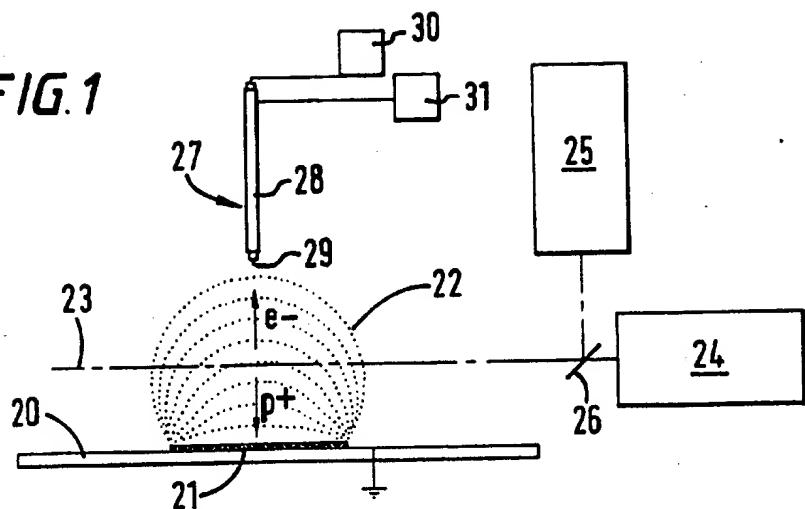
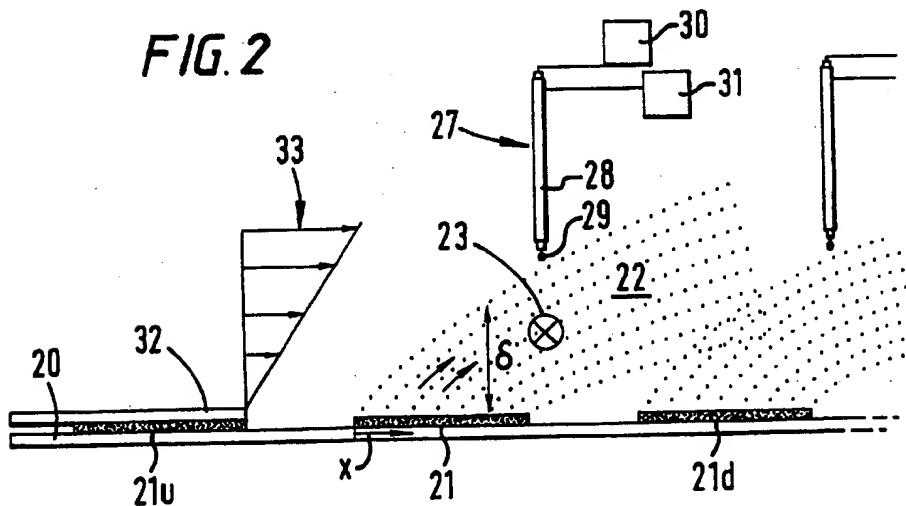
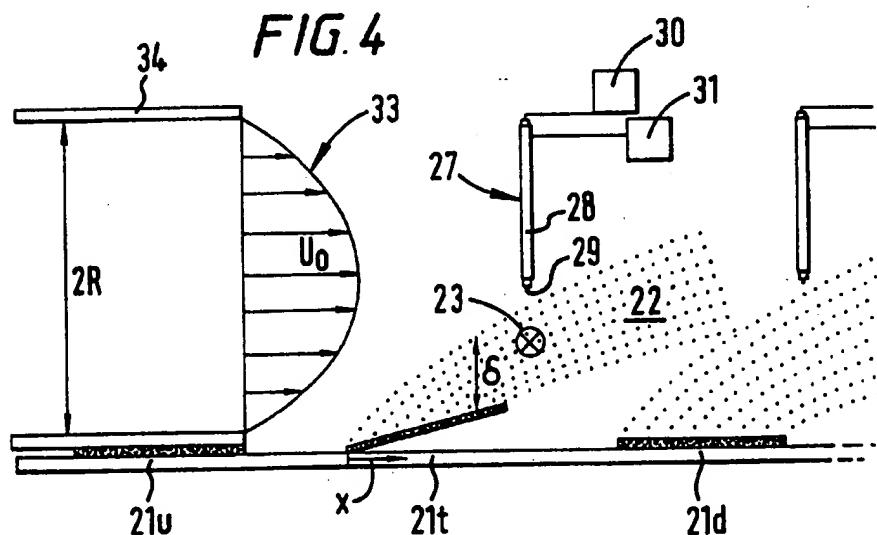
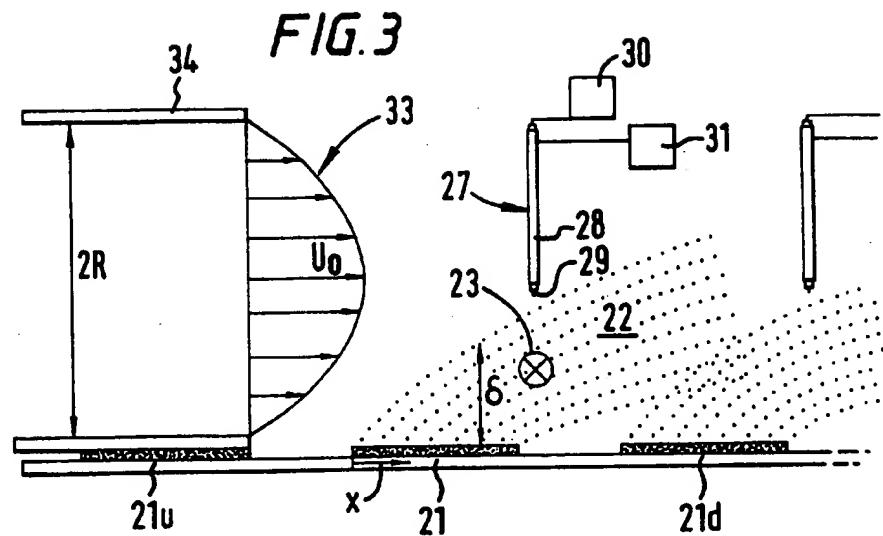


FIG. 2



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FIG. 5

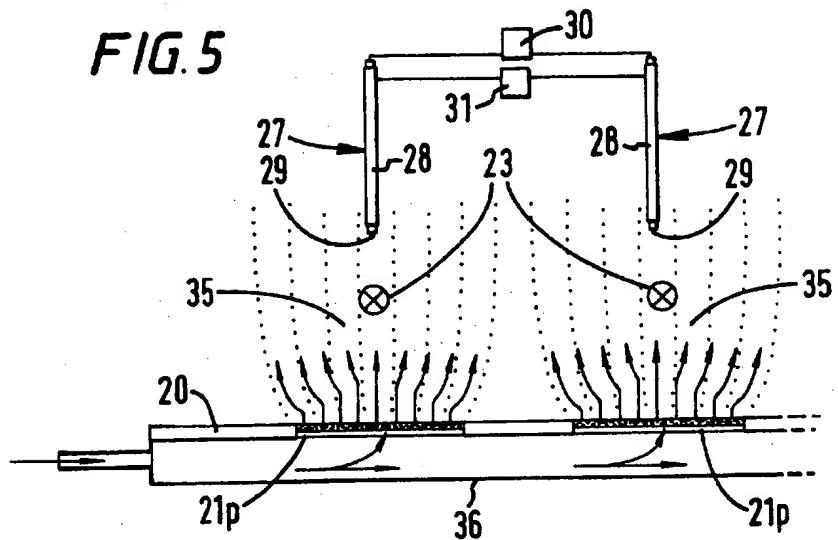
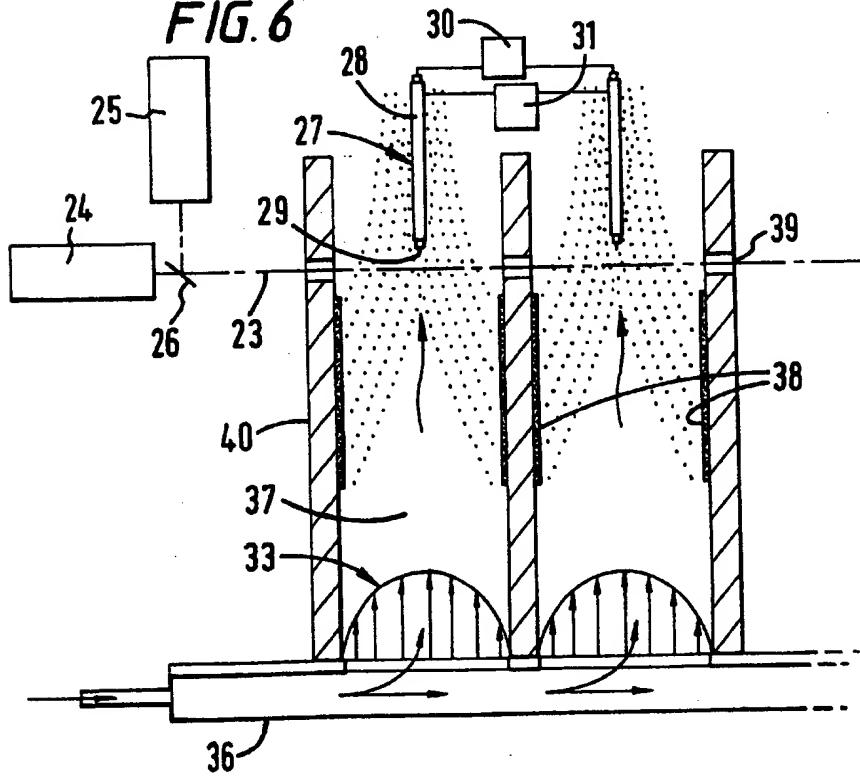


FIG. 6



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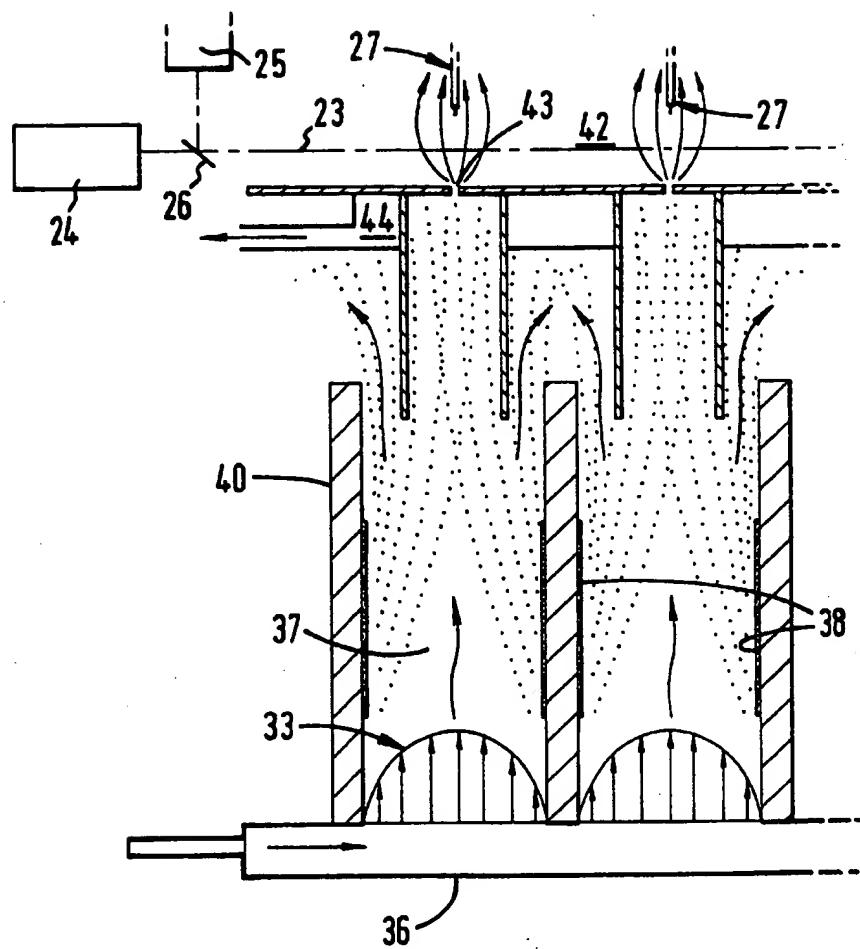
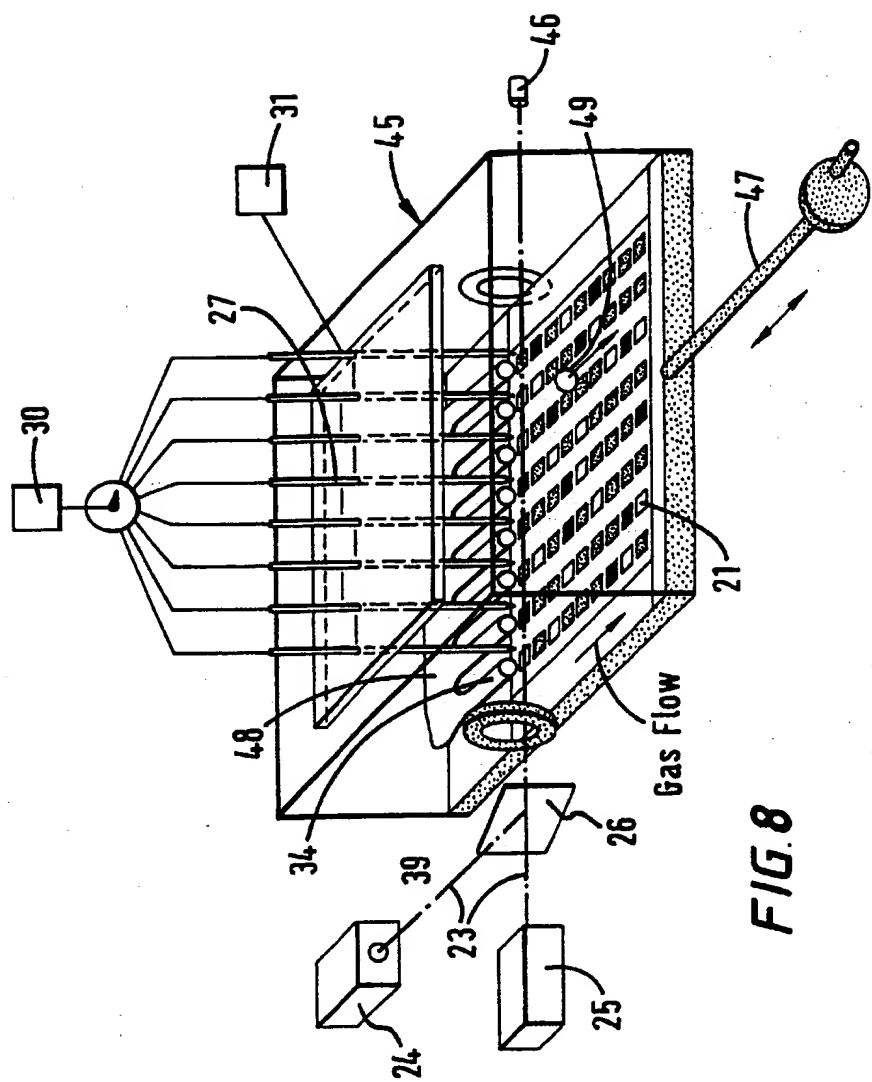


FIG. 7

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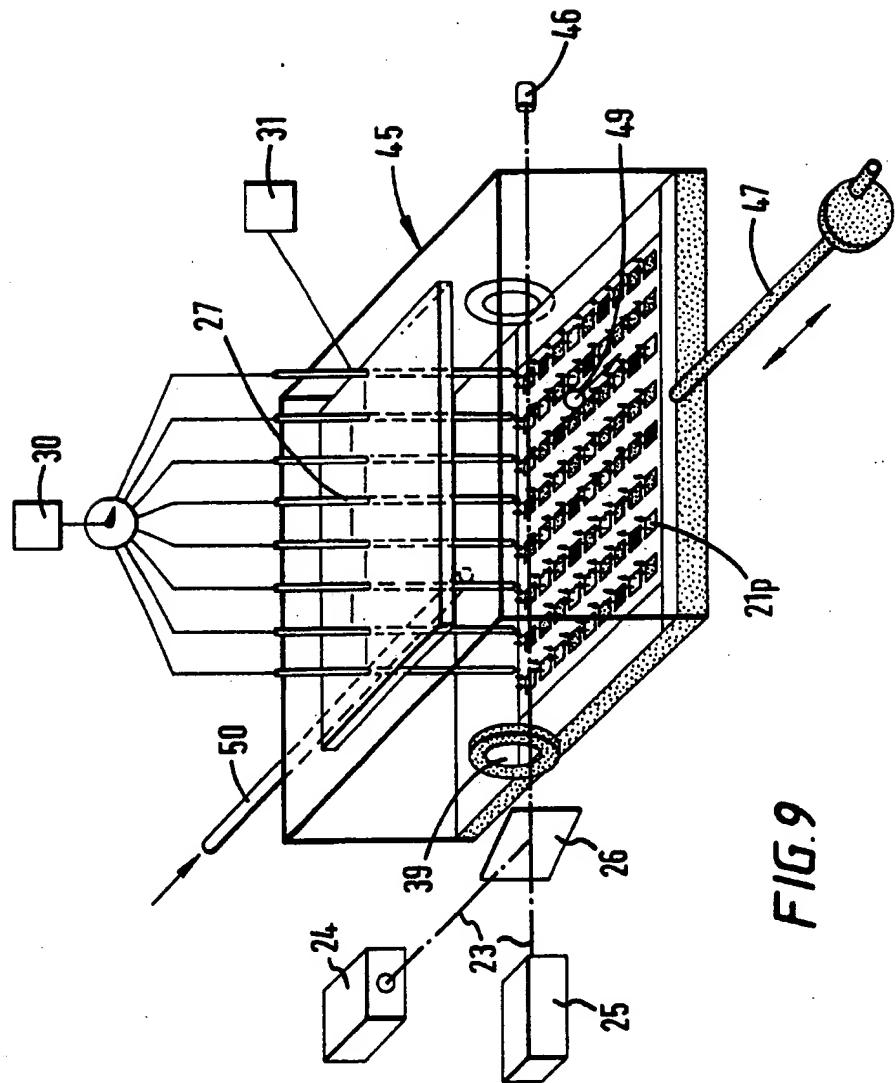
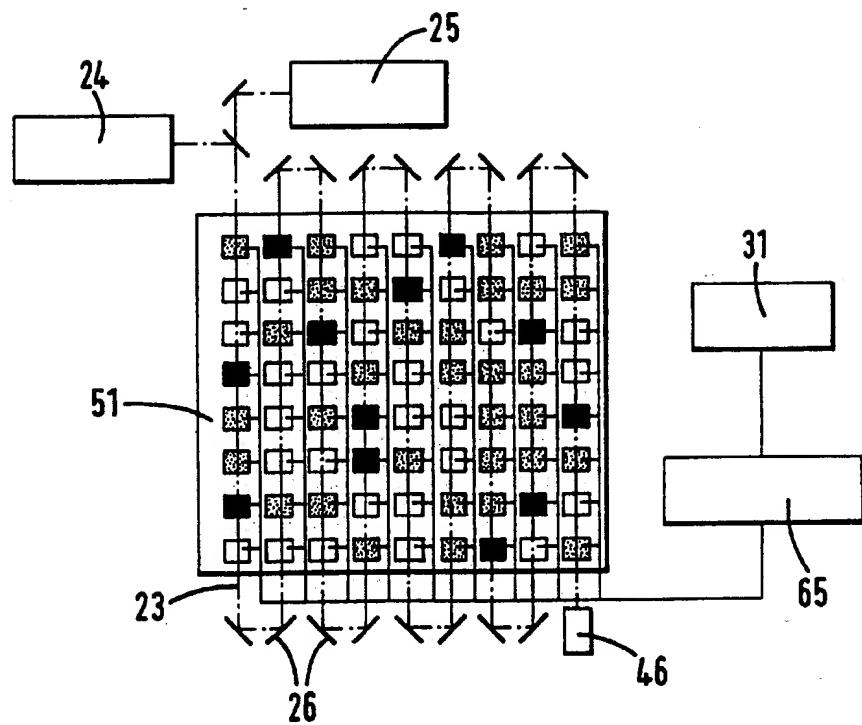


FIG. 9

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FIG. 10



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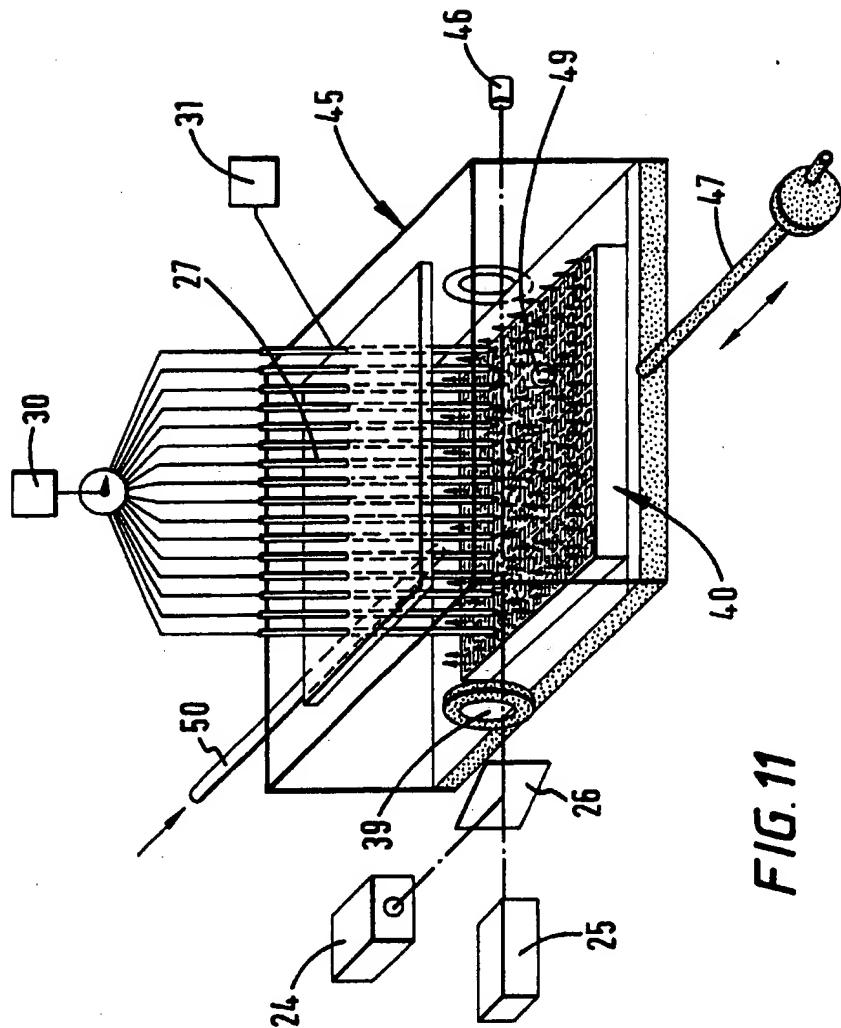


FIG. 11

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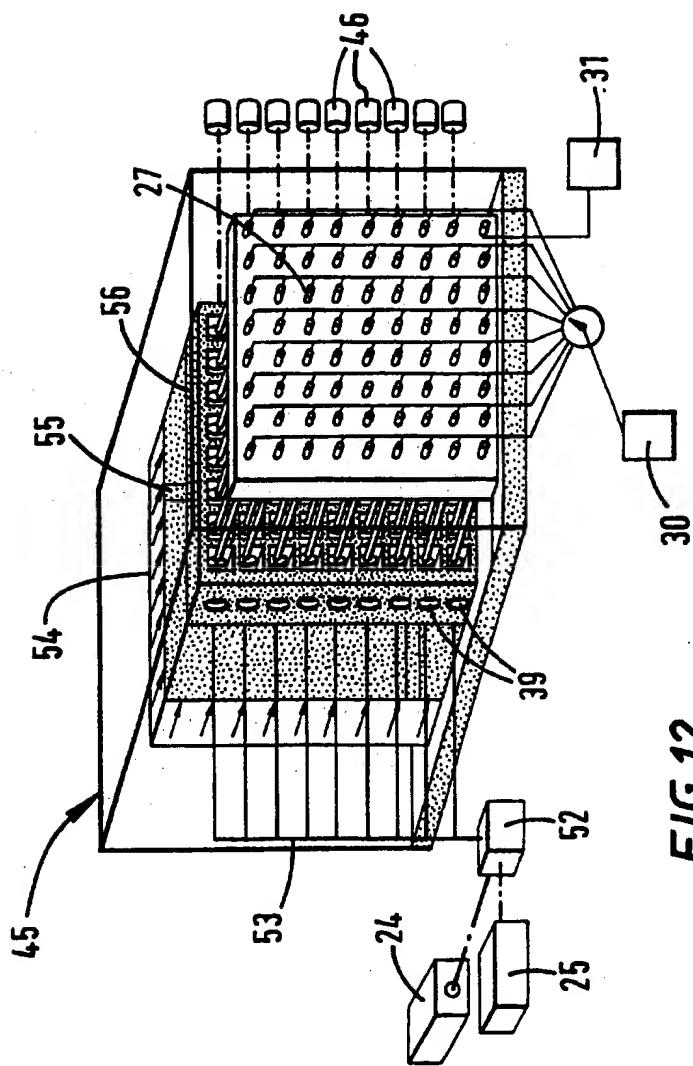
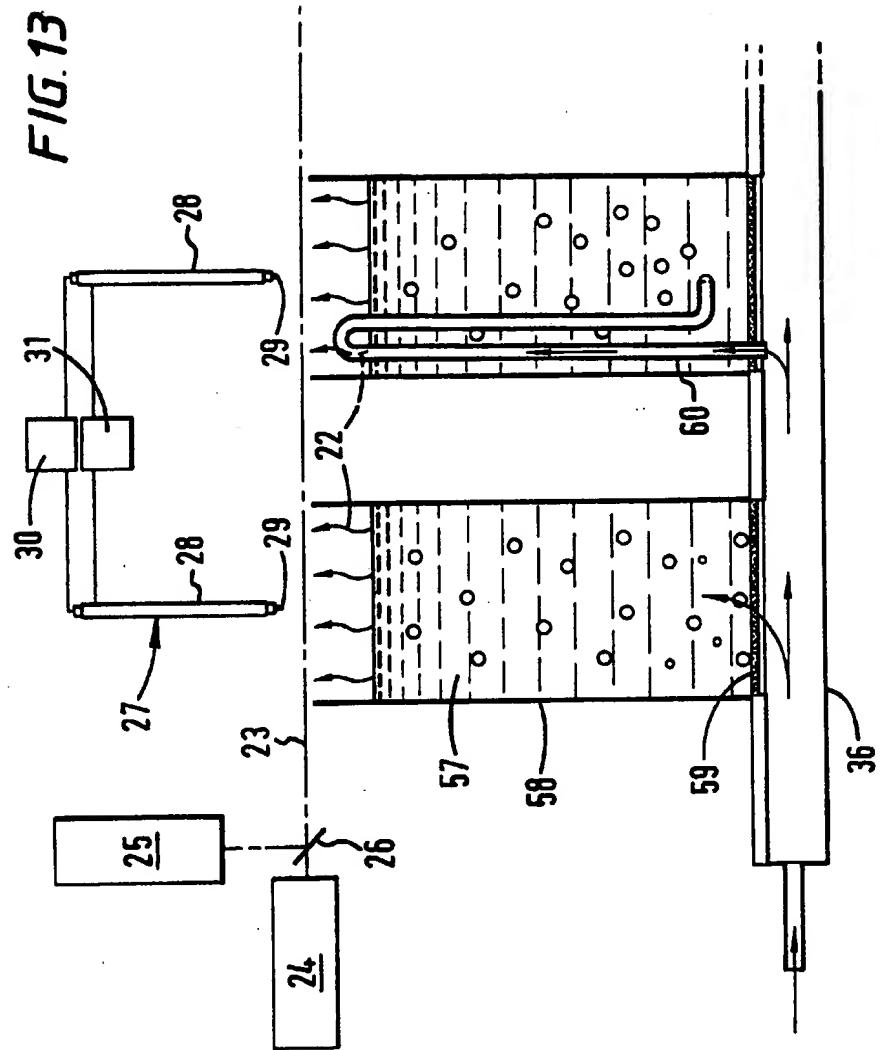


FIG. 12

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FIG. 13



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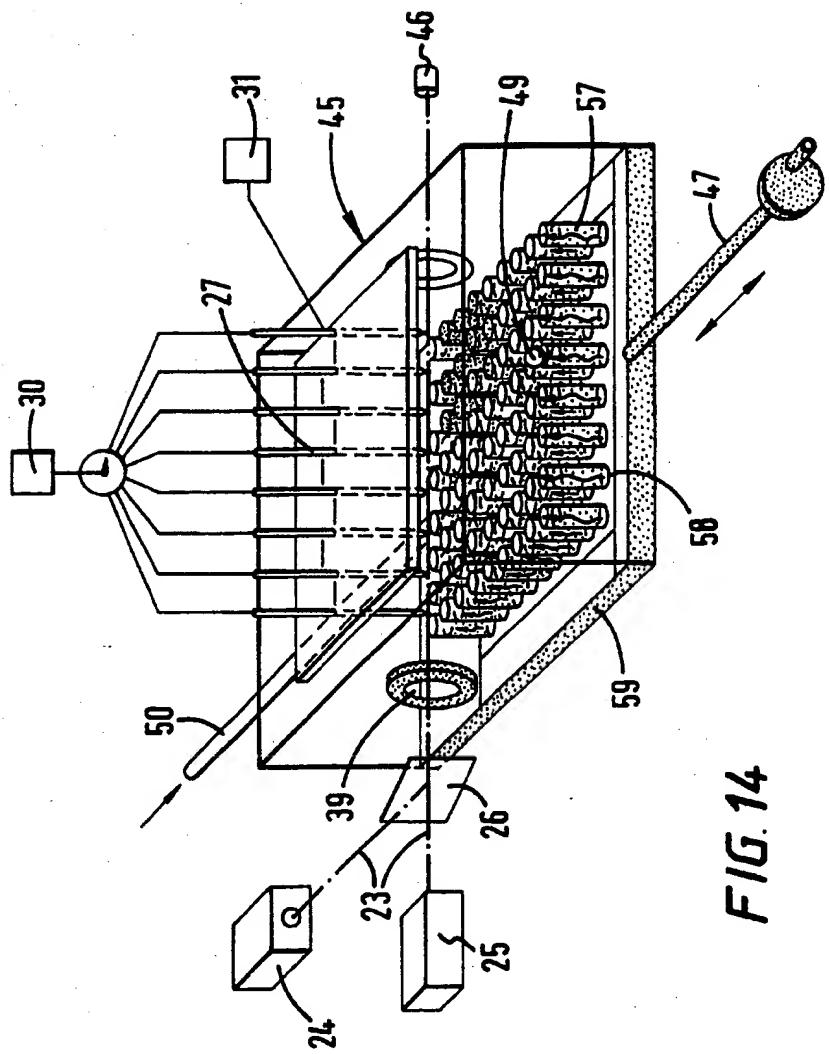


FIG. 14

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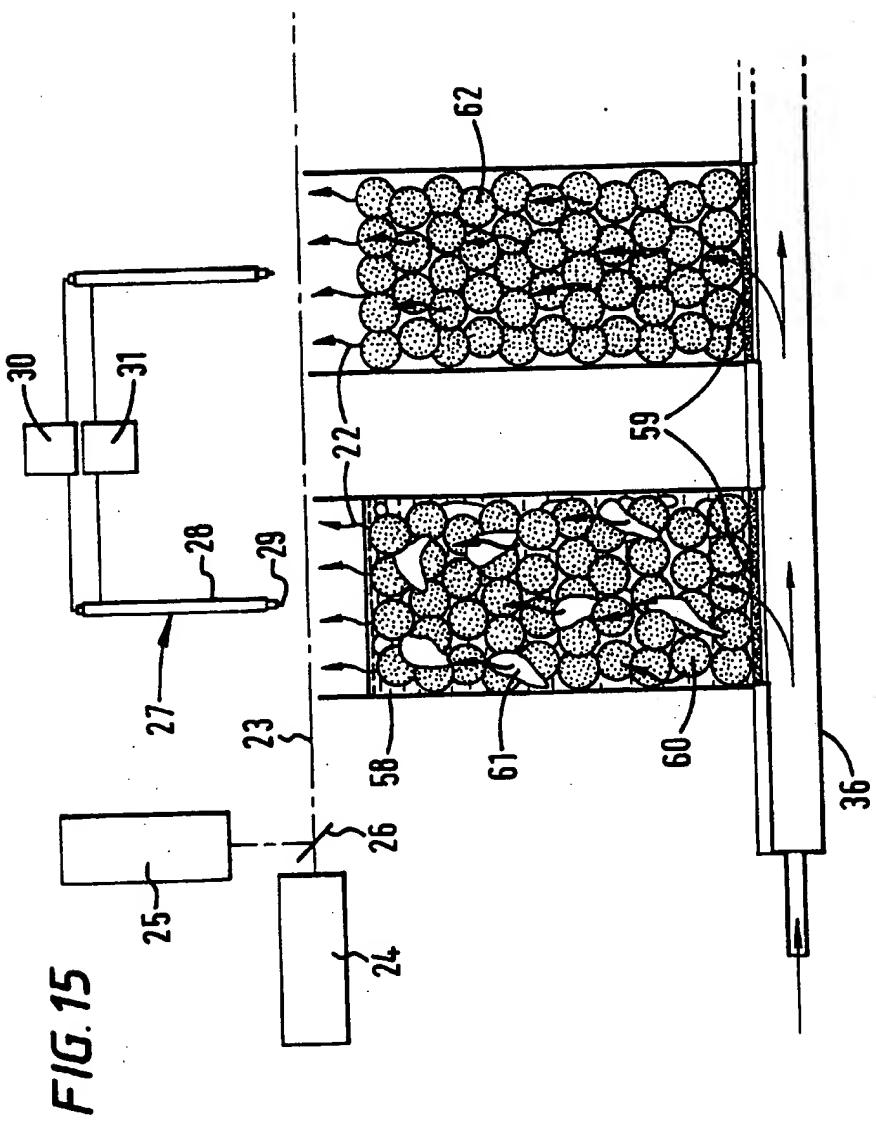
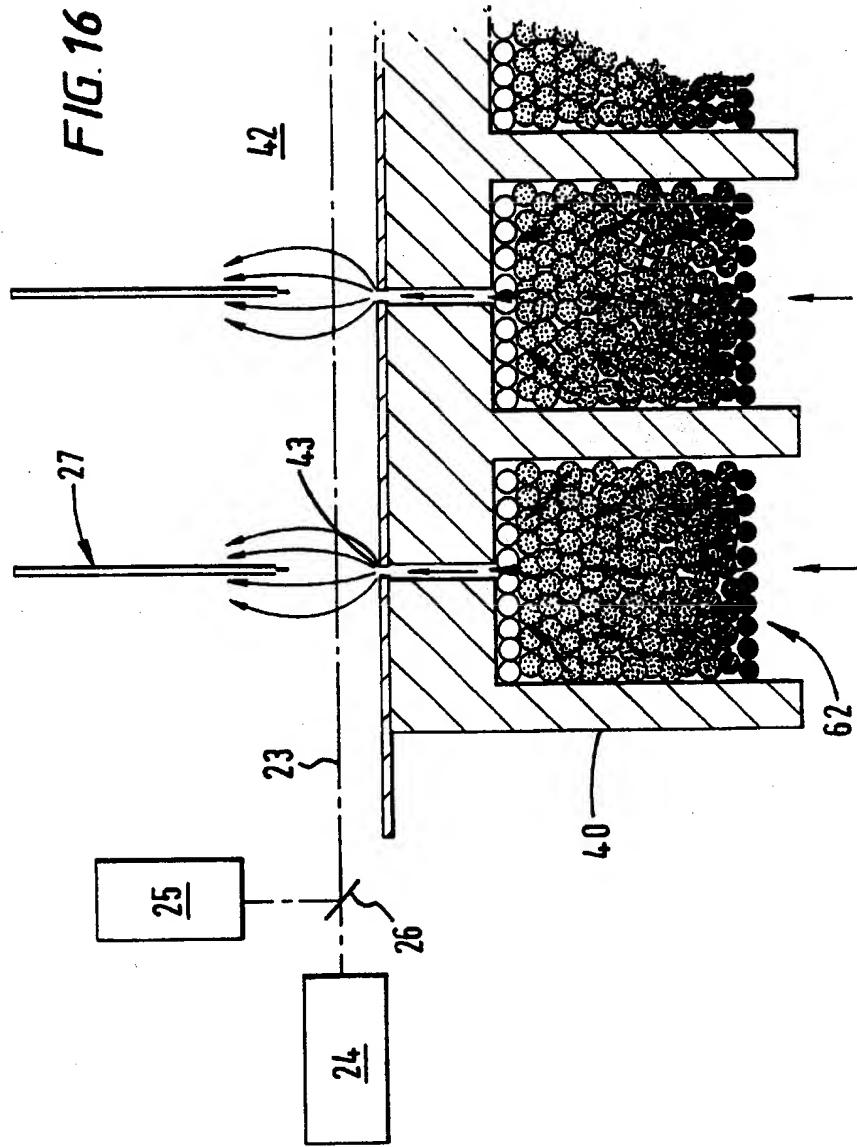


FIG. 15

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FIG. 16



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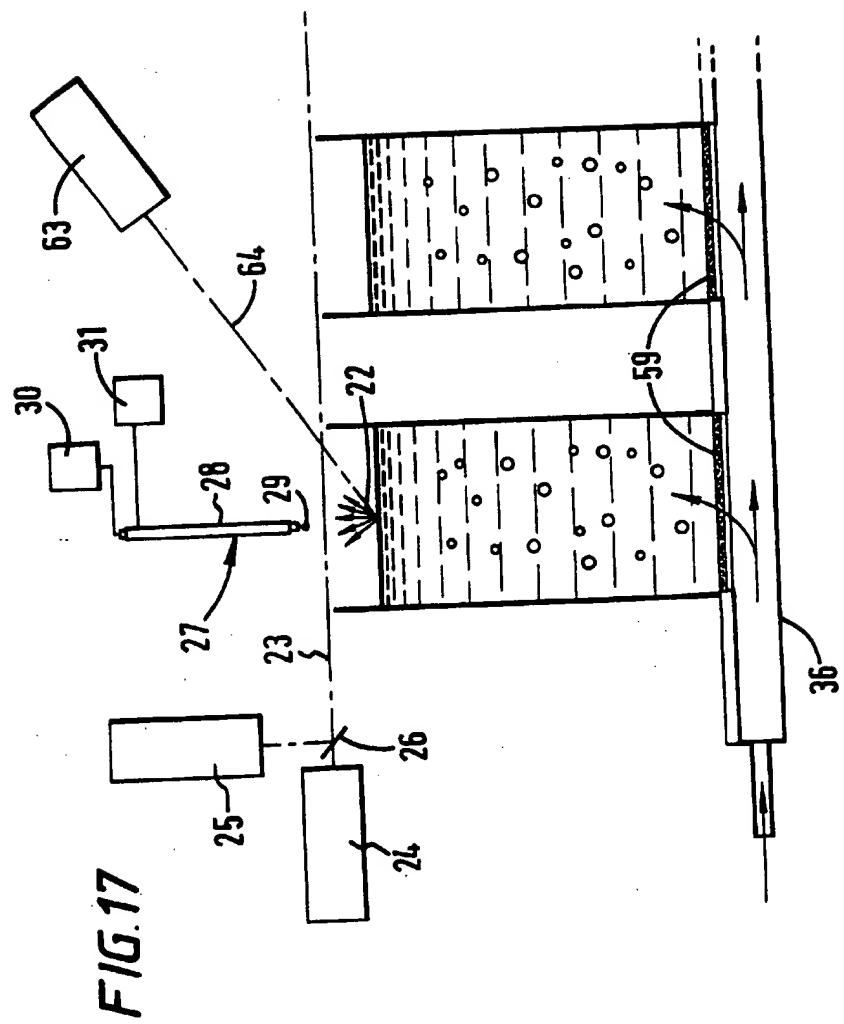
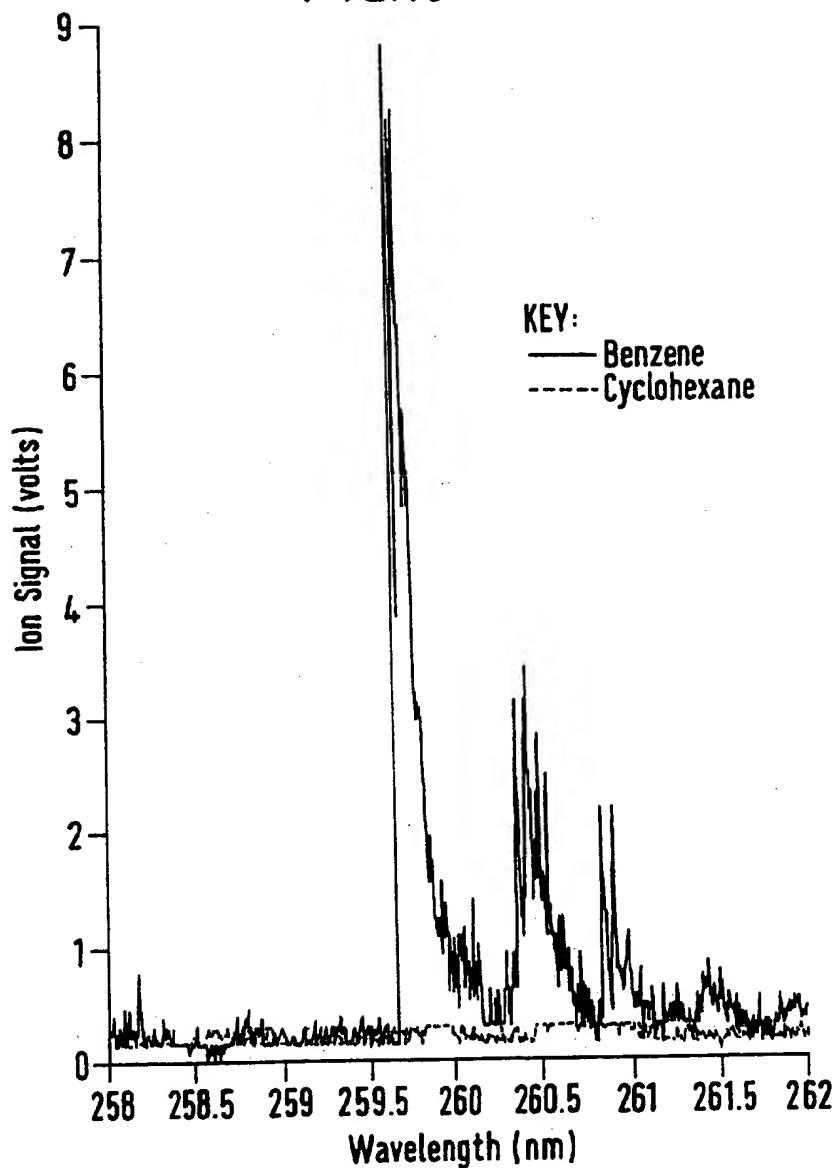


FIG. 17

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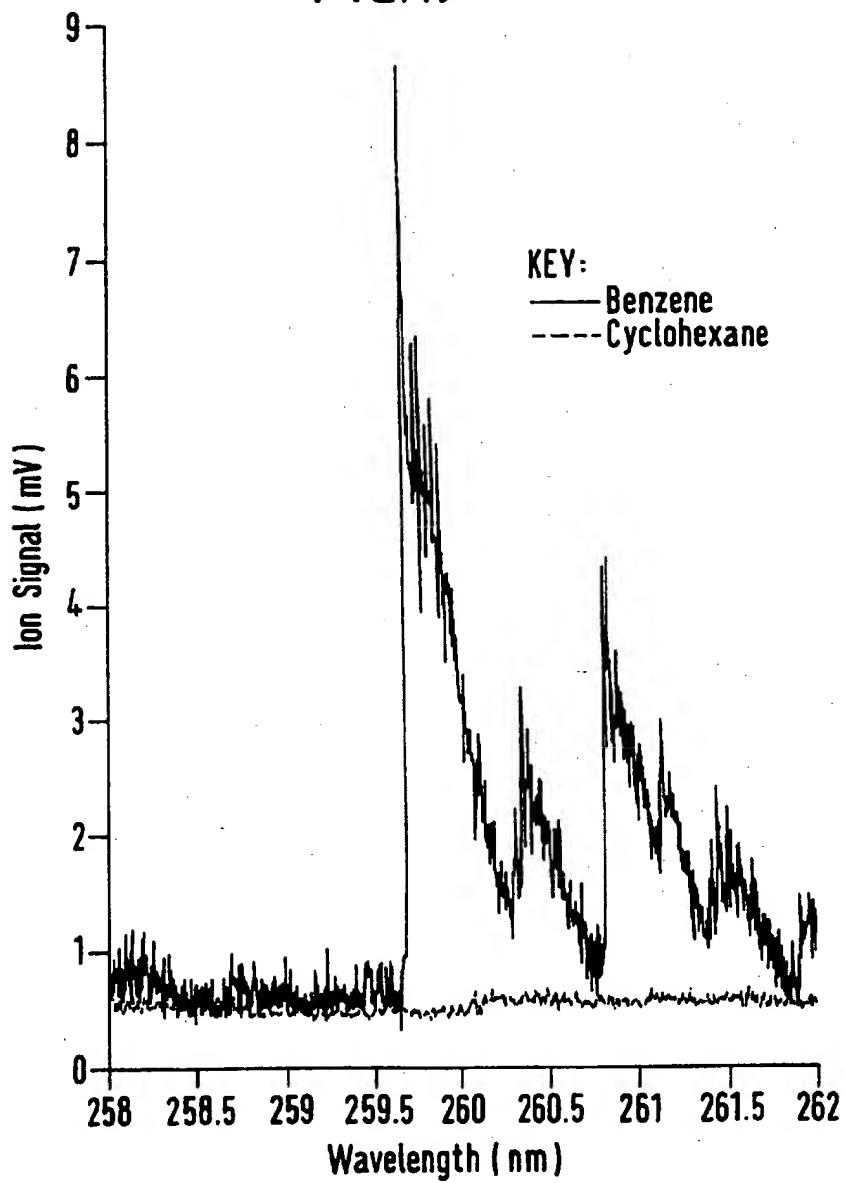
FIG. 18



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FIG. 19



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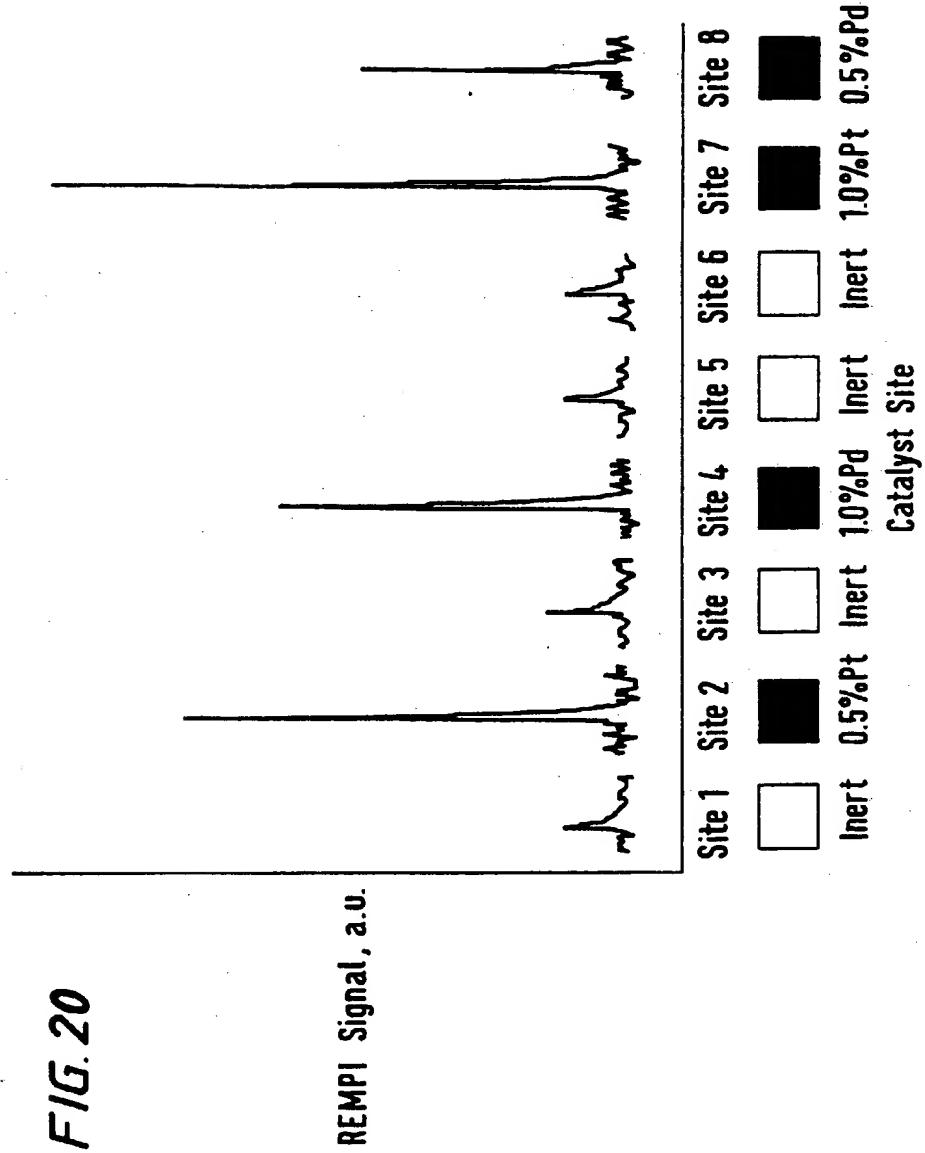


FIG. 20

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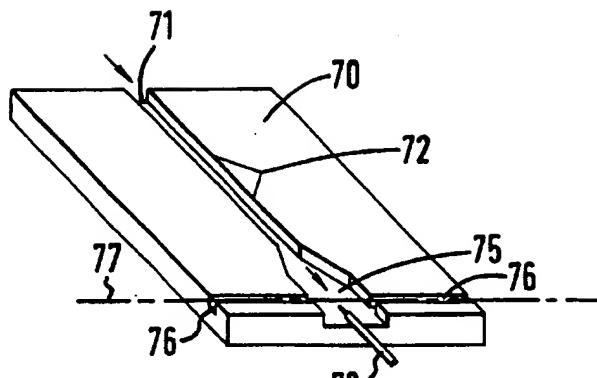


FIG. 21

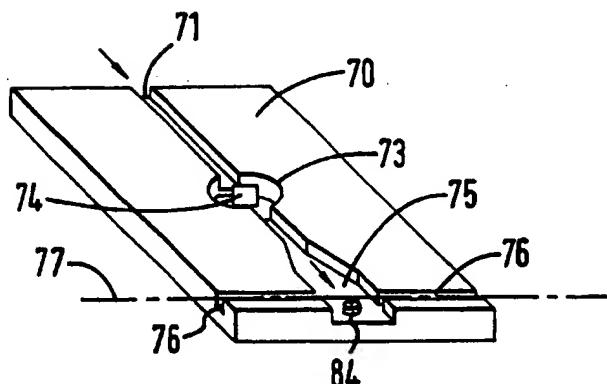


FIG. 22

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FIG. 23

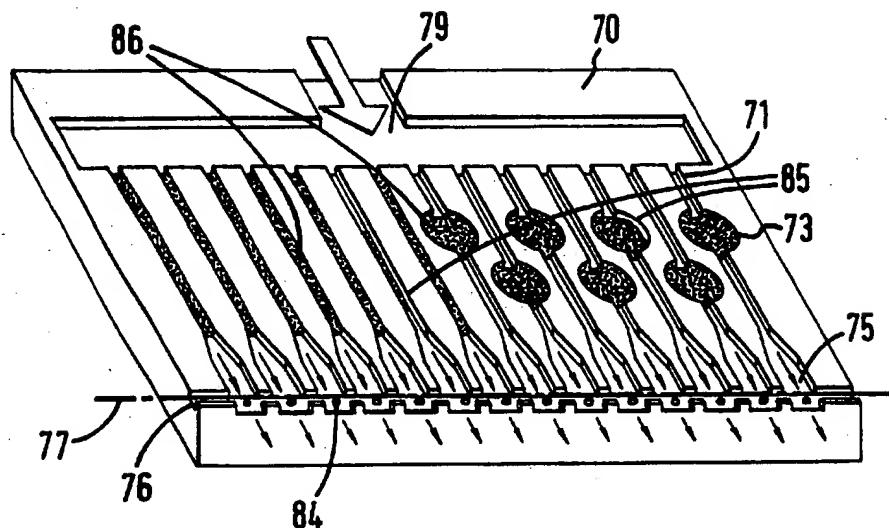
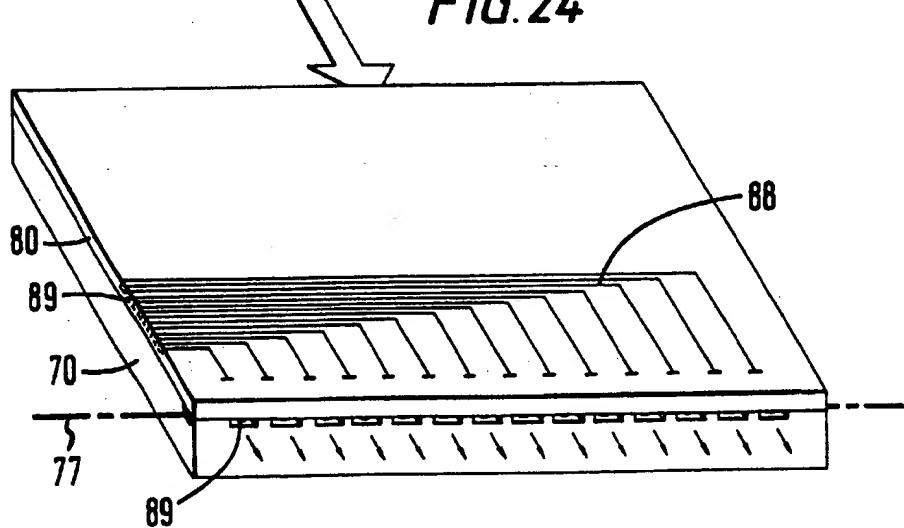
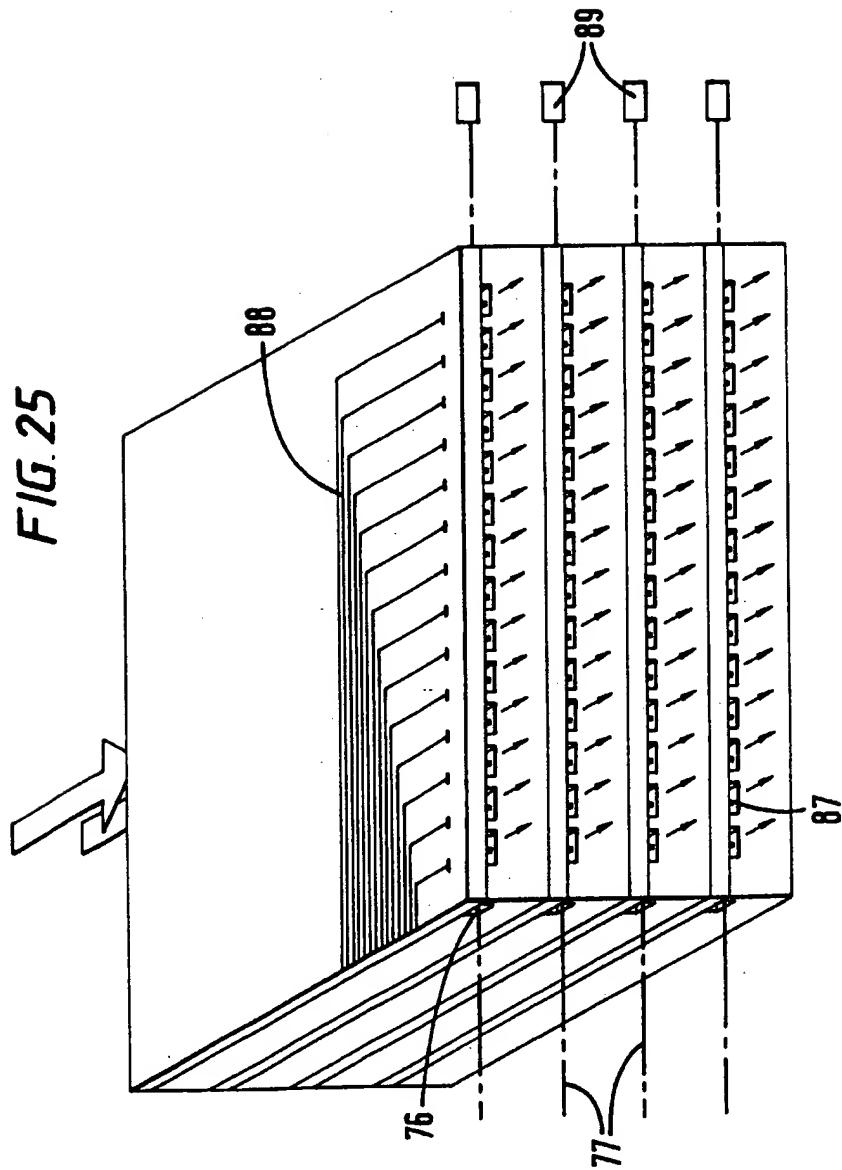


FIG. 24



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FIG. 26

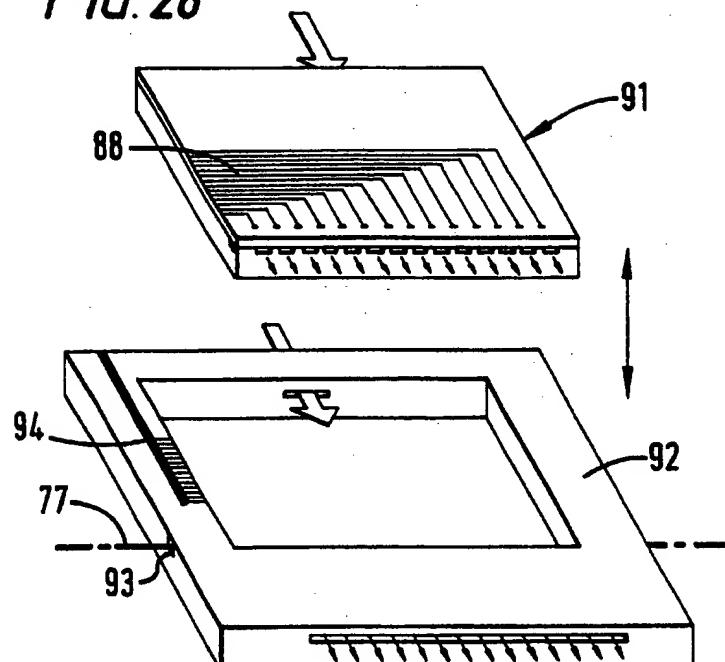
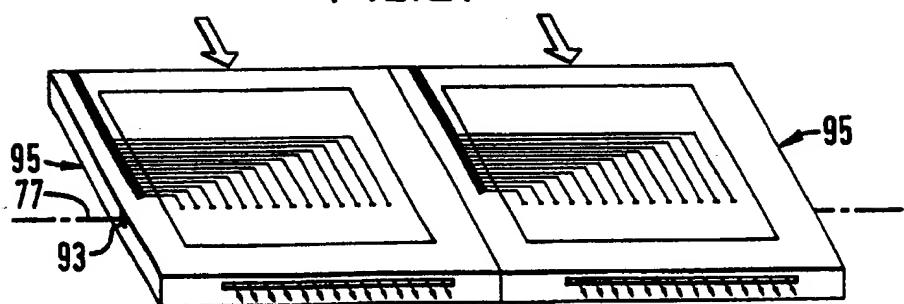
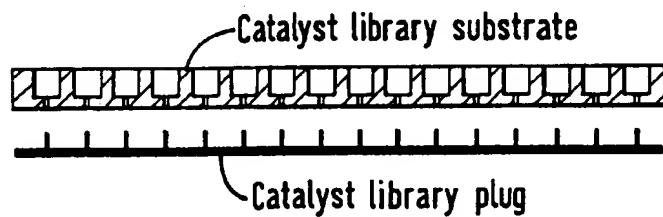
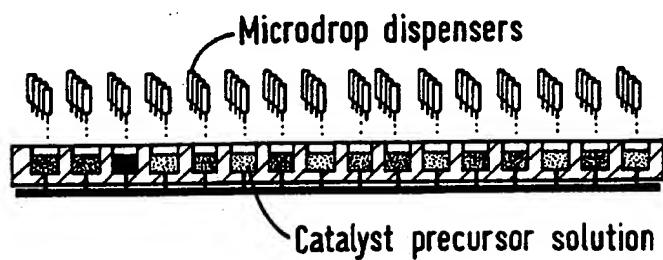
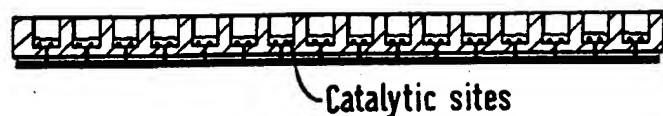


FIG. 27

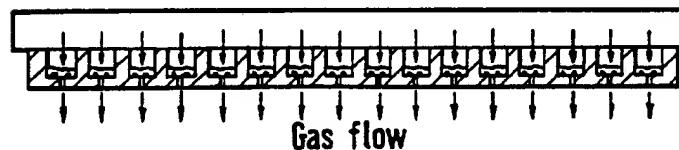
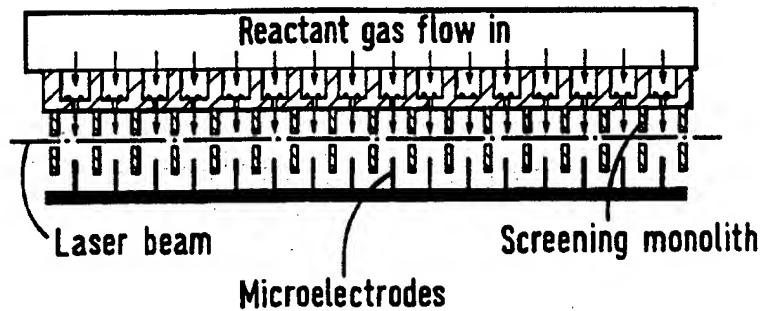


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FIG. 28A**STEP 1 - Library Substrate Preparation.****STEP 2 - Precursor Solution Deposition.****STEP 3 - Drying and Calcination.**

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FIG. 28B**STEP 4 - Removal of the Library Plug.****STEP 5 - Activation.****STEP 6 - Screening.**

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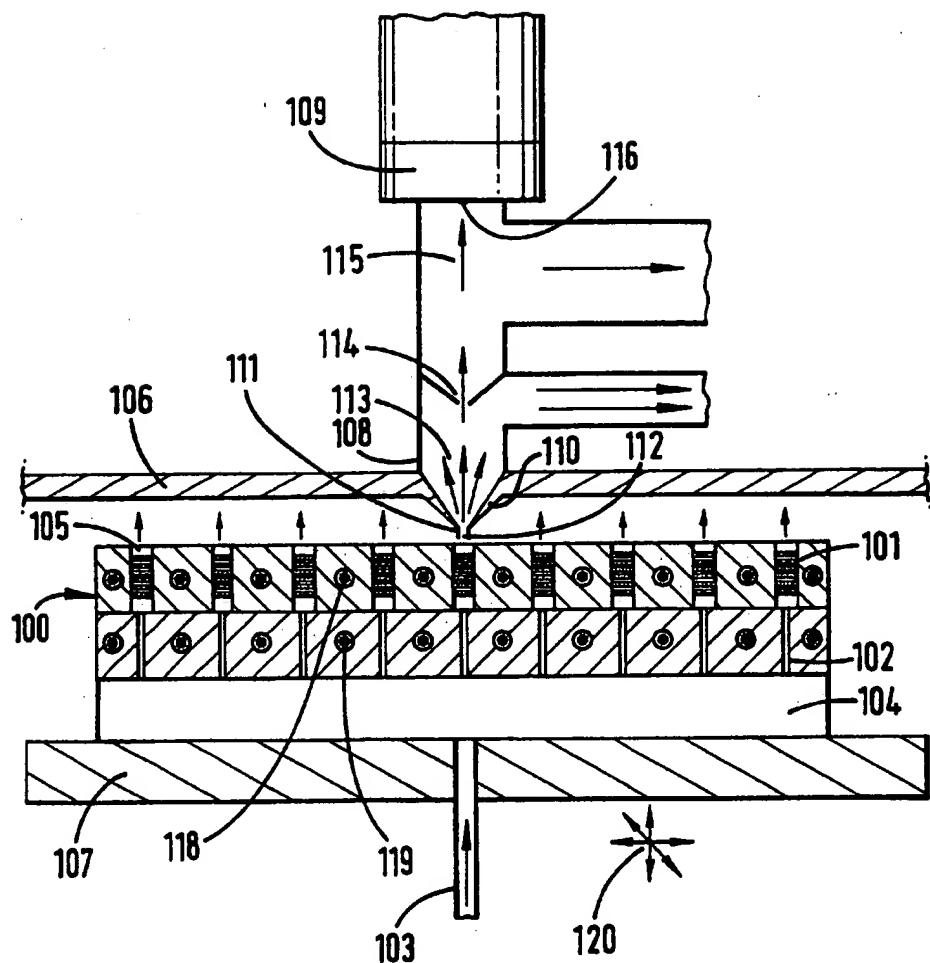
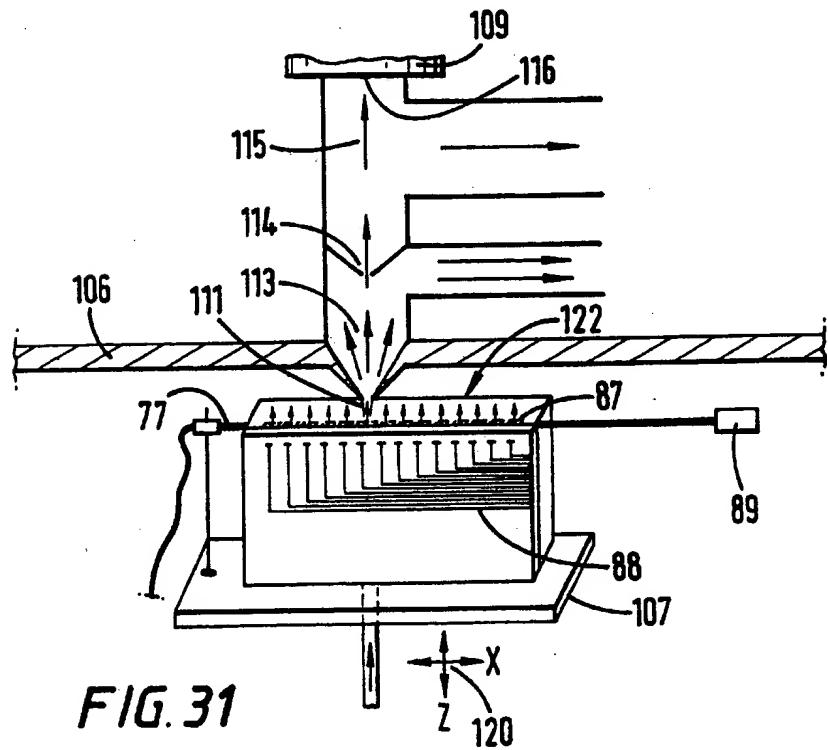
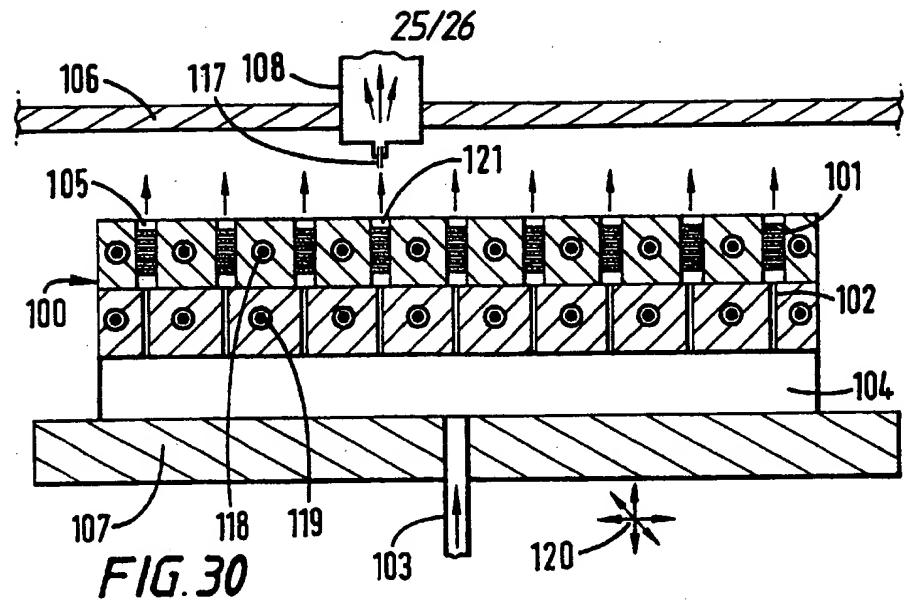


FIG. 29



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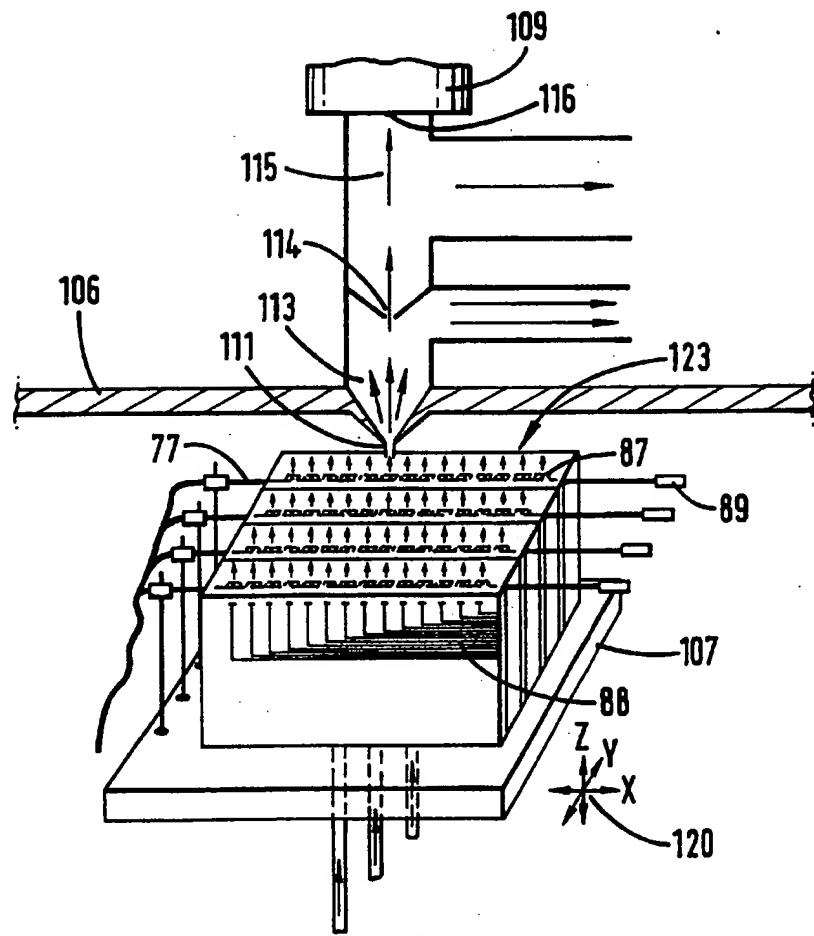


FIG. 32

INTERNATIONAL SEARCH REPORT

Int'l Serial Application No
PCT/GB 99/03767A. CLASSIFICATION OF SUBJECT MATTER
IPC 7 G01N33/00 G01N31/10 G01N27/62

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
IPC 7 G01N

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the International search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	EP 0 266 334 A (MONSANTO CO) 4 May 1988 (1988-05-04) column 14, line 40 -column 15, line 20; figure 1 column 21, line 14-28	1,6,10, 12,17
Y	WO 97 32208 A (TECHNOLOGY LICENSING CO L L C ;WILLSON RICHARD COALE III (US)) 4 September 1997 (1997-09-04) page 2, line 14 -page 6, line 25	1,6,10, 12,17
A	WO 98 15501 A (SYMYX TECHNOLOGIES) 16 April 1998 (1998-04-16) page 3, line 28 -page 6, line 3	1,8-10, 12,20 -/-

 Further documents are listed in the continuation of box C. Patent family members are listed in annex.

* Special categories of cited documents :

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